



A Multi-scale Computational Framework for Property Prediction of Fluid Mixtures

March 7-9, 2023



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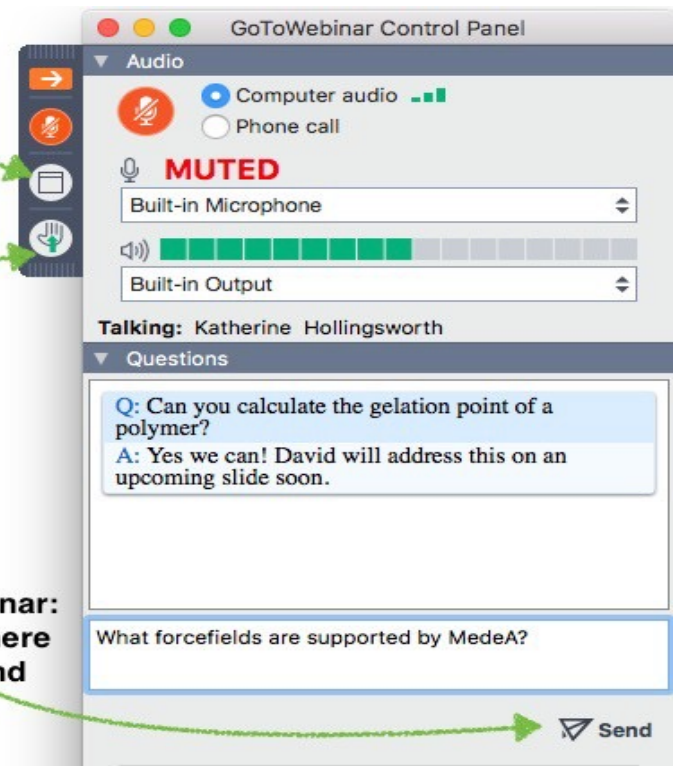
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Webinar Speakers

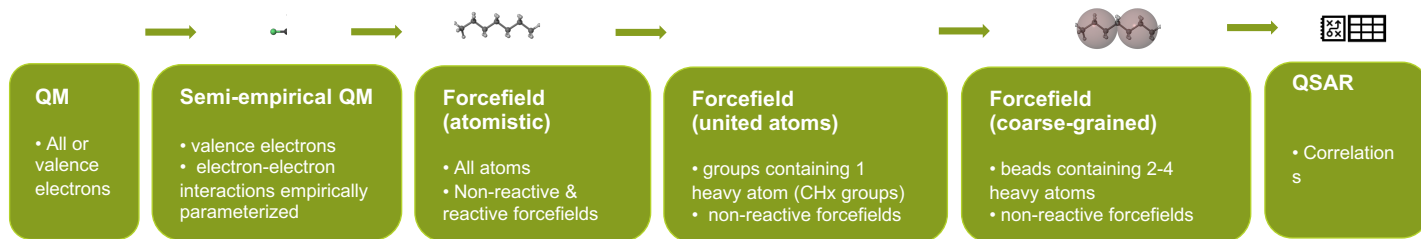
Katherine Hollingsworth

Presenter: Dr. Marianna Yiannourakou

How can molecular modeling help?

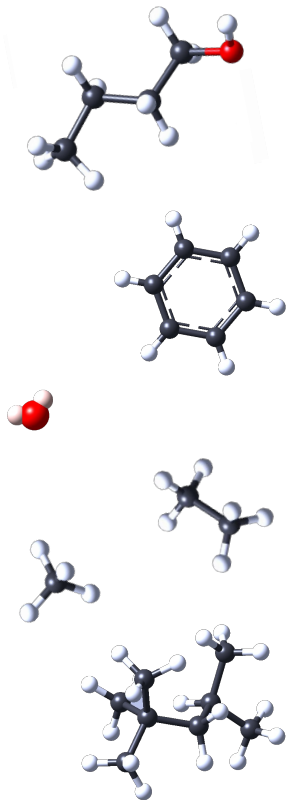
- What properties can be calculated using molecular modeling?
- How are the properties calculated?
- What is the expected accuracy for property prediction of fluid mixtures, using molecular modeling?
- What input is required?
- What is the computation cost and human effort for the computations?

Tools: Different levels of description



- Simulations at different levels of theory, using corresponding models can be used to study phenomena that occur at different time/length scales
- Selection of the appropriate level of theory and methods depends on:
 - Property or phenomenon of interest
 - Expected accuracy
 - Method coverage
- Information from one level can be passed on to the next

Fluids

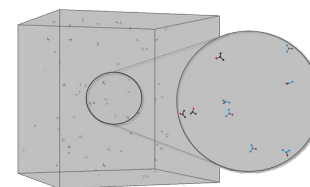
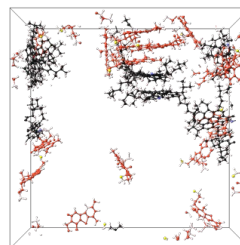
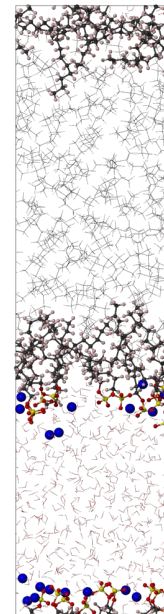


Pure Compounds' Properties

- 1 Density
- 2 Saturation Pressure
- 3 Vaporization Enthalpy
- 4 Chemical potential / Fugacity
- 5 Cohesive Energy Density
- 6 Joule-Thomson Coefficient
- 7 Speed of Sound
- 8 Heat Capacity
- 9 Compressibility Factor
- 10 Normal Boiling Point Temperature
- 11 Critical Point (density, pressure, temperature)
- 12 Heat of Formation
- 13 IR Spectra
- 14 UV-Vis Spectra
- 15 Multipole moments (dipole, quadrupole, etc)
- 16 Self Diffusion Coefficient
- 17 Thermal Conductivity
- 18 Viscosity
- 19 Surface Tension
- 20 Acentric factor
- 21 Thermal expansion coefficient

Mixtures' Properties

- 1 Density
- 2 Equilibrium Pressure
- 3 Chemical Potential / Fugacity
- 4 Composition
- 5 Equilibrium constants
- 6 Henry solubility constant
- 7 Azeotrope
- 8 Joule-Thomson Coefficient
- 9 Speed of Sound
- 10 Heat Capacity
- 11 Self Diffusion Coefficient
- 12 Thermal Conductivity
- 12 Viscosity
- 13 Thermal expansion coefficient



Calculating fluid mixtures properties from molecular simulations

All-atom / United-Atom / Coarse-Grained Forcefields

- VLE
- Henry Solubility constants
- Diffusivity coefficients
- Viscosity
- Surface Tension

Fluid Phase Equilibria 560 (2022) 113478



Contents lists available at [ScienceDirect](#)

Fluid Phase Equilibria

journal homepage: www.elsevier.com/locate/fluid

Molecular simulations for improved process modeling of an acid gas removal unit

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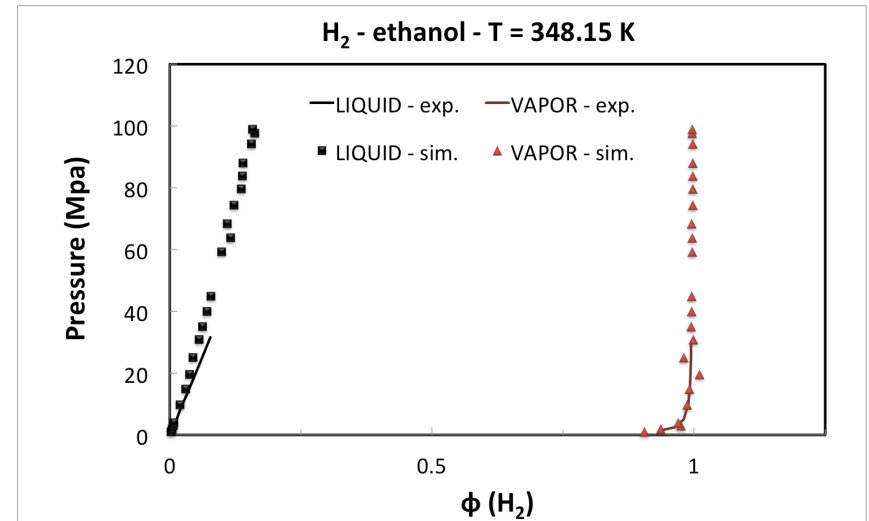
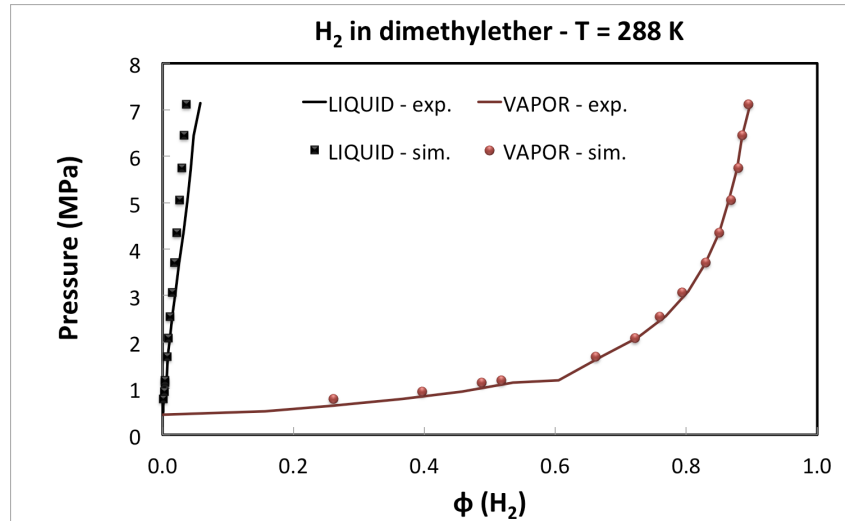
^cMINES ParisTech, PSL University, Centre de Thermodynamique des Procédés (CTP), 35 rue St Honoré, 77300 Fontainebleau, France

Forcefields (FF)

1. All-atom (AA, non-reactive) FFs for organics (and some inorganics), e.g.:
 - PCFF+ (used in the MD examples shown here)
 - PCFF+ has a coverage of 97% of the compounds contained in the DIPPR's Project 801 Database
2. United-Atom (UA, non-reactive) FFs for organics, e.g.:
 - AUA+ (used in the MC examples here)
 - Several popular models for small molecules, such as H₂S, CO₂, H₂O, CH₄
3. SAFT- γ Mie (CG, non-reactive) FFs for organics:
 - Developed from SAFT EOS
 - Coverage of 6000+ compounds and possibility to parametrize from both bottom-up and top-bottom approaches: www.bottledsaft.org

Vapor Liquid Equilibria - Mixtures

MedeA GIBBS simulations

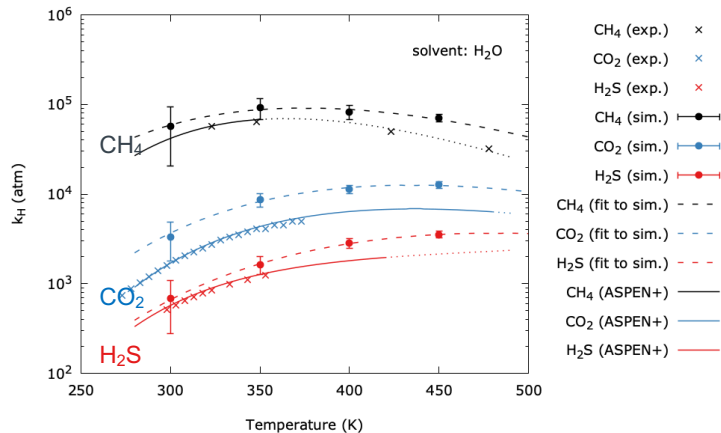


Yiannourakou et al., *Mol. Sim.* 39, p. 1165-1211 (2013)

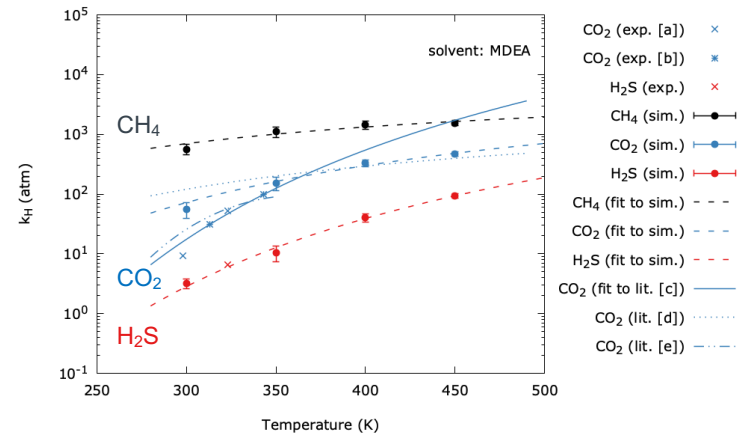
Henry Solubility Constant

- Simulations accurately predict Henry solubility constants ranking and temperature dependence
- Semi-quantitative agreement is achieved (order of magnitude) for all three solutes in water

Yiannourakou *et al.*, *Molecular simulations for improved process modeling of an acid gas removal unit*, FPE 560, p. 113478 (2022)



Monte Carlo simulations in the Gibbs Ensemble (*Medea GIBBS*)



Monte Carlo simulations in the Gibbs Ensemble (*Medea GIBBS*)

Left plot:

- Exp. data for CO₂/H₂S/ CH₄ from:
 - Gillespie *et al.*, Gas Processors Association. (1982)
 - Carroll *et al.*, J. Phys. Chem. Ref. Data 20, p. 1201 (1991); Crovetto *et al.*, J. Phys. Chem. Ref. Data 20, p. 575 (1991); Prini *et al.*, J. Phys. Chem. Ref. Data 18, p. 1231 (1989)
 - Iliuta *et al.*, J. Chem. Eng. Data 52, p. 2 (2007); Sander, Atmos. Chem. Phys. 15, p. 4399 (2015)

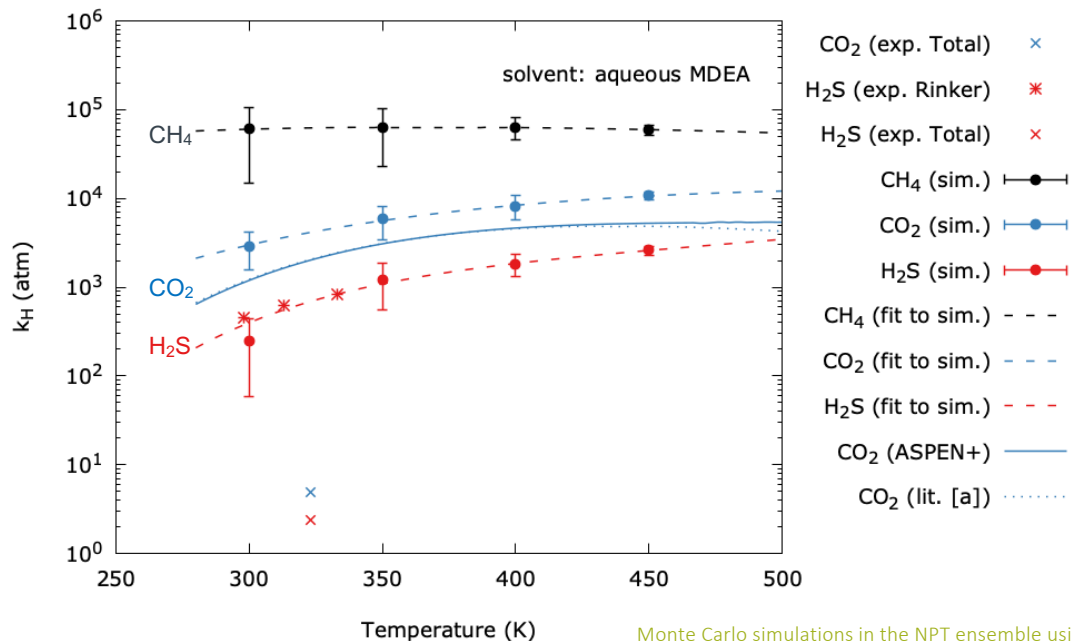
•12 CO₂ / CH₄ / H₂S (ASPEN+): ASPEN+

Right plot:

- Exp. data for CO₂ [a] / H₂S from: TotalEnergies, Internal data (2019)
- Exp. data for CO₂ [b]: Skylogianni *et al.* (2020)
- CO₂ (lit [c]): Skylogianni *et al.* (2020)
- CO₂ (lit [d]): Zhang & Chen (2011)
- CO₂ (lit [e]): TotalEnergies, Internal data (2019)

Henry Solubility Constant

- Aqueous solution of MDEA: 30% wt
- Simulations results for H₂S are in agreement with experiments reporting measuring only physisorption of H₂S in MDEA, using a protonated MDEA solution
- Simulation results for CO₂ overpredict the Henry constant (underestimate the solubility) of CO₂ in MEDEA but accurately predict the temperature dependence of the Henry constant



Monte Carlo simulations in the NPT ensemble using Widom test insertions (Medea GIBBS)

- Exp. TOTAL: TotalEnergies (2019) – unpublished work
- Exp. Sandal: Rinker *et al.*, The Canadian J. of Chem. Eng. 78 (2000)
- CO₂ (ASPEN+): ASPEN+
- CO₂ (lit): Zhang *et al.*, Ind. & Eng. Chem. Res. 50, p. 163 (2011)

Yiannourakou *et al*, Molecular simulations for improved process modeling of an acid gas removal unit, FPE 560, p. 113478 (2022)

Diffusivity

Self-Diffusion Coefficient

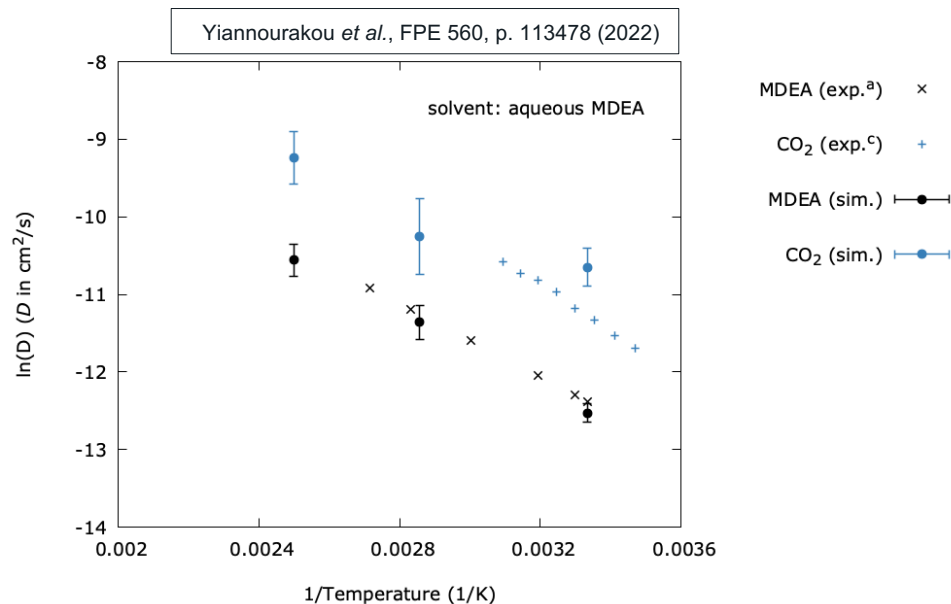
- Run NVE simulations and calculate the Mean Squared Displacement of the molecules

$$MSD = \left\langle (r(t) - r(t_0))^2 \right\rangle$$

$r(t)$ and $r(t_0)$ are the position vectors of the gas molecule i at times t and t_0 , respectively; Brackets $\langle \rangle$ denote the ensemble average over time origins, providing the mean square displacement (MSD)

- Calculate the self-diffusion coefficient of the molecules through their MSD

$$D = \frac{1}{6} \cdot \frac{\left\langle (r(t) - r(t_0))^2 \right\rangle}{t}$$



Equilibrium molecular dynamics simulations in the NVE ensemble (Medea LAMMPS)

- Exp. MDEA (a): Snijder *et al.*, *Journal of Chemical & Engineering Data*. 38, p. 475-480 (1993)
- Exp. CO₂ (c): Al-Ghawas *et al.*, *Journal of Chemical & Engineering Data* 34, p. 385-391 (1989)

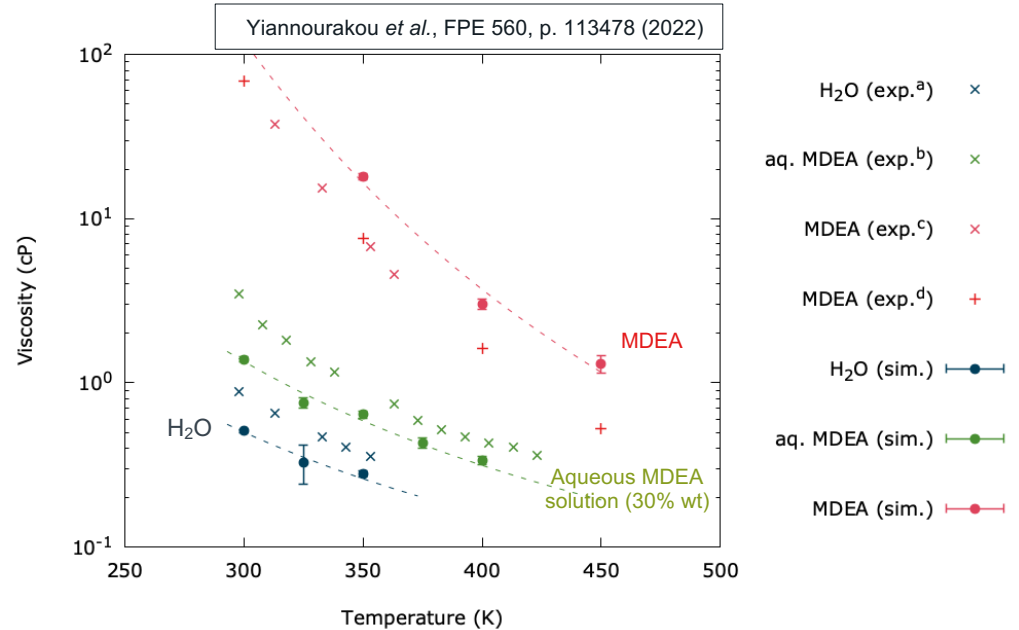
Viscosity of water, MDEA and an aqueous solution of MDEA

- The Green-Kubo method is used for the calculation of viscosity during equilibrium molecular dynamics (EMD) simulations

$$\eta = \frac{V}{kT} \int_0^{\infty} \langle P_{ij}(0)P_{ij}(t) \rangle dt$$

where V is the volume of the cell, k the Boltzmann's constant, T is the temperature, P_{ij} , $i, j = x, y, z$ are components of the shear stress tensor

- Calculated viscosities of MDEA and the aqueous solution of MDEA (30% wt) predict the temperature dependence of the viscosity



Equilibrium molecular dynamics simulations in the NVE ensemble (*MedeA LAMMPS*)

- Exp. H₂O (a): Teng *et al.*, J. Chem. Eng. Data 39, p. 290 (1994)
- Exp. aqueous MDEA solution (30% wt) (b): Arachchige *et al.*, Ann. Trans. Of the Nordic Rheol. Soc. 22 (2014)
- Exp. MDEA (c): Yusoff *et al.*, J. Ind. & Eng. Chem. 20, p. 3349 (2014)
- Exp. MDEA (d): Wilding *et al.*, Dippr project 801, FPE 150-151, p. 413 (1998)

Surface Tension of water, methanol and their mixtures

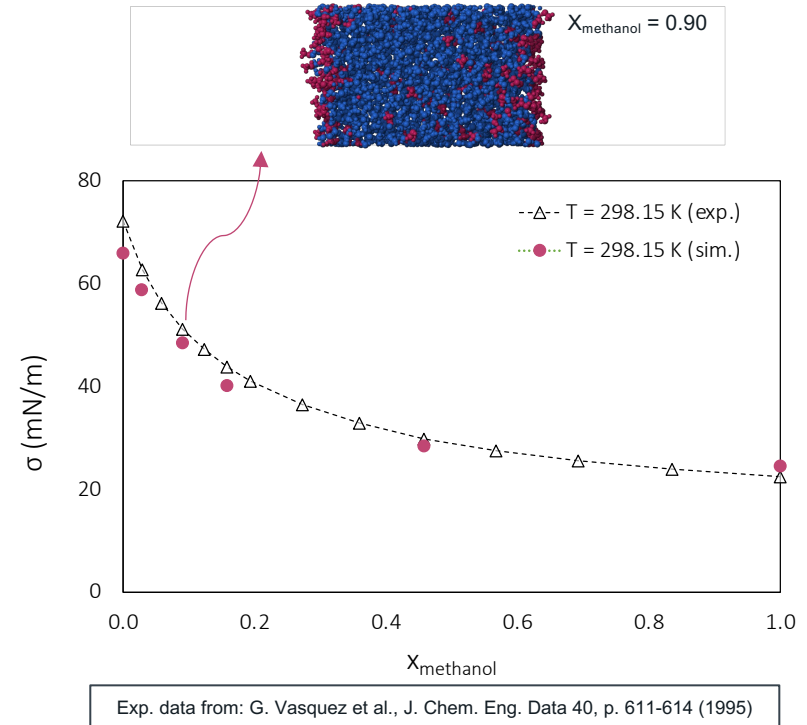
- Calculation of surface tension during MD simulations in the NVT ensemble

$$\gamma = 0.5L \left\{ \langle \sigma_z \rangle - \frac{1}{2} [\langle \sigma_x \rangle + \langle \sigma_y \rangle] \right\}$$

where L is the cell length in the direction normal to the interface and brackets $\langle \rangle$ denote the time average

- Qualitatively and quantitatively, the results agree well with experimental data
- Simulation details:
 - Forcefield: pcff+ (v2023)
 - Each point is the average of five (5) consecutive simulations of duration 1 ns each
 - System size: 2,000 molecules (water & ethanol)
 - $T = 298.15$ K
 - $r_{\text{cut}} = 15 \text{ \AA}$
 - $t_{\text{step}} = 1$ fs

Equilibrium molecular dynamics simulations in the NVT ensemble (*Medea LAMMPS*)



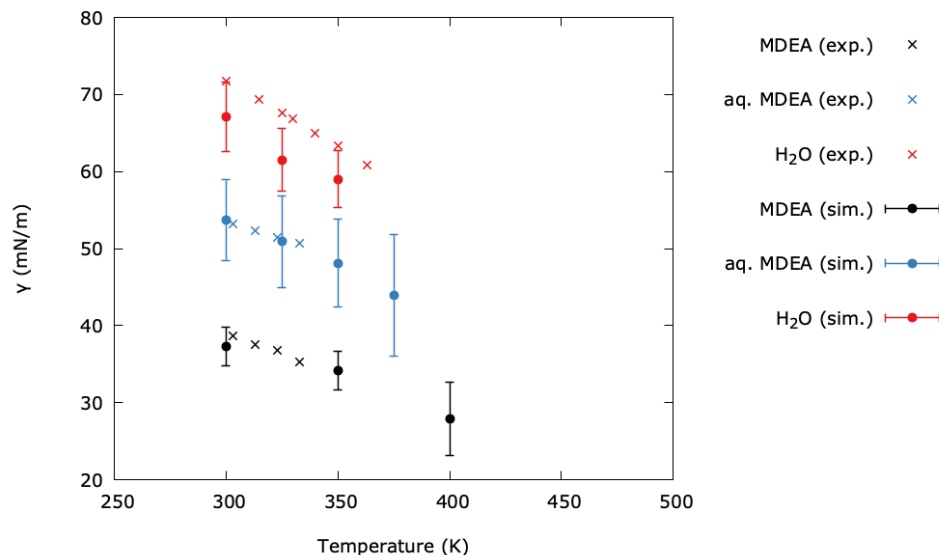
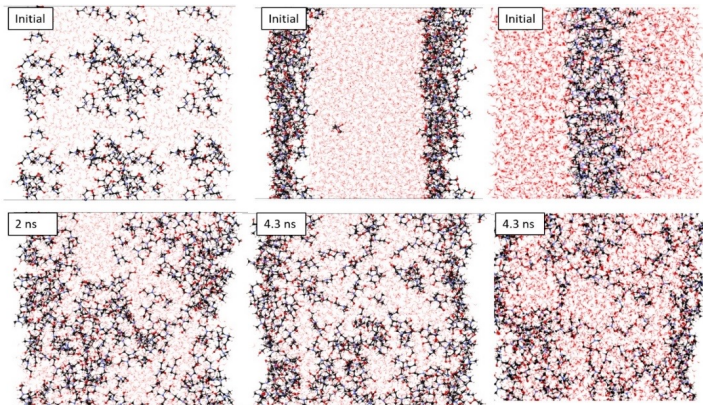
Surface Tension of water, MDEA and an aqueous MDEA solution

- Calculation of surface tension during MD simulations in the NVT ensemble

$$\gamma = 0.5L \left\{ \langle \sigma_z \rangle - \frac{1}{2} [\langle \sigma_x \rangle + \langle \sigma_y \rangle] \right\}$$

where L is the cell length in the direction normal to the interface and brackets $\langle \rangle$ denote the time average

- Qualitatively and quantitatively, the results agree well with experimental data for MDEA, H₂O and the aqueous solution of MDEA (30% wt)





Yiannourakou *et al.*, FPE 560, p. 113478 (2022)

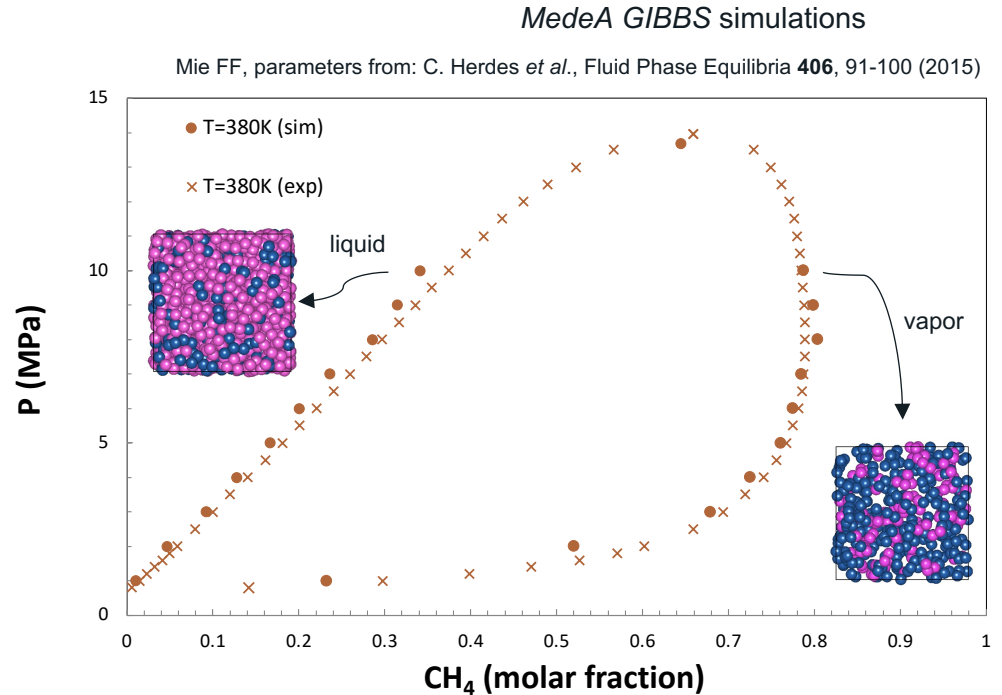
Equilibrium molecular dynamics simulations in the NVT ensemble (*Medea LAMMPS*)

- Exp. MDEA: Wilding *et al.*, Dippr project 801, FPE 150-151, p. 413 (1998)
- Exp. aqueous MDEA solution (30% wt): Muhammad *et al.*, J. Chem. & Eng. Data 53, p. 2226 (2008)
- Exp. H₂O: Vargaftik, Volkov, & Voljak, 1983

VLE of mixtures – Coarse grained models

methane / n-pentane

- $T = 380 \text{ K}$
- $P \in [1, 10] \text{ MPa}$
- Isobaric GEMC simulations
- 40 million steps
- 800-1000 molecules
- methane: 1 bead 
- n-pentane: 2 beads 



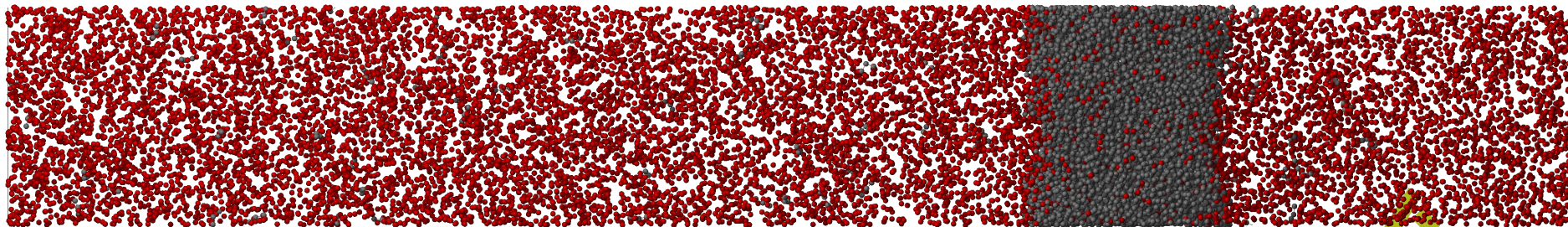
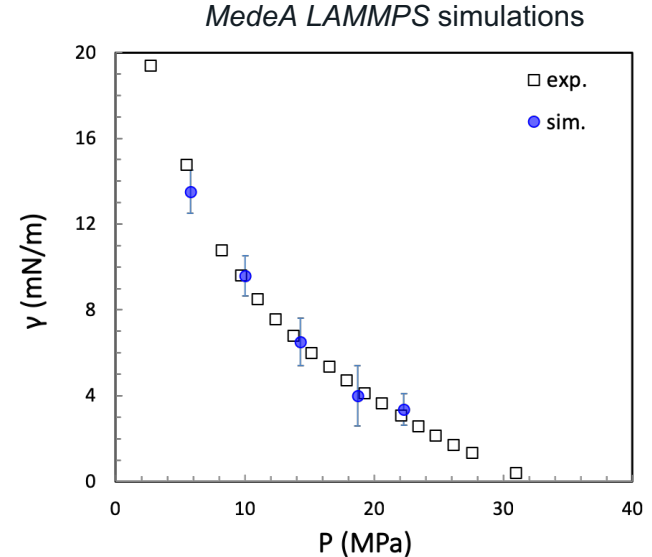
Exp. Data from: V.M. Berry and B.H. Sage, "Phase Behavior in Binary and Multicomponent Systems At Elevated Pressures: n-Pentane and Methane-n-Pentane"

Interface Tension – Coarse-grained description

methane / n-decane

- $T = 366.48 \text{ K}$
- $P \in [5, 25] \text{ MPa}$
- $t_{\text{step}} = 0.01 \text{ ps}$
- $t = 5 \text{ ns}$

Reproduction of work from:
C. Herdes *et al.*, *Fluid Phase Equilibria*
406, 91-100 (2015)



Calculating fluid mixtures properties from correlations

- Density

Compositional Modeling of Crude Oils Using C₁₀–C₃₆ Properties Generated by Molecular Simulation

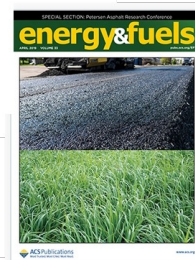
Philippe Ungerer*, Marianna Yiannourakou, Alexander Mavromaras, and Julien Colletl

✓ Cite this: *Energy Fuels* 2019, 33, 4, 2967–2980

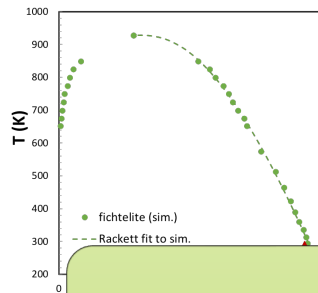
Publication Date: March 4, 2019

<https://doi.org/10.1021/acs.energyfuels.8b04403>

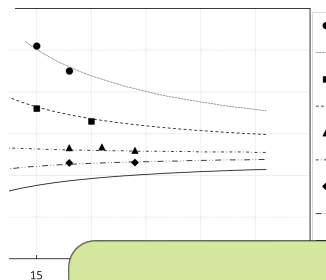
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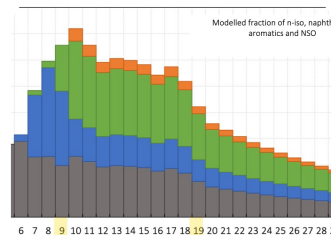
Summary



Calculation of
pure-compound
properties



Calculation of
correlations for
pure-compounds



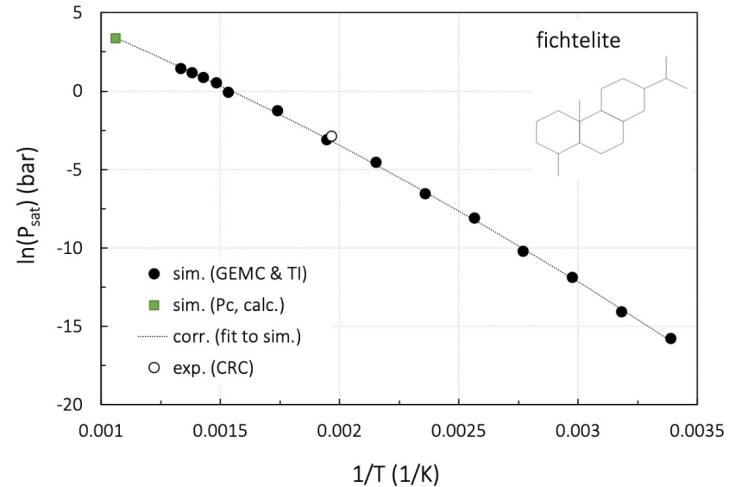
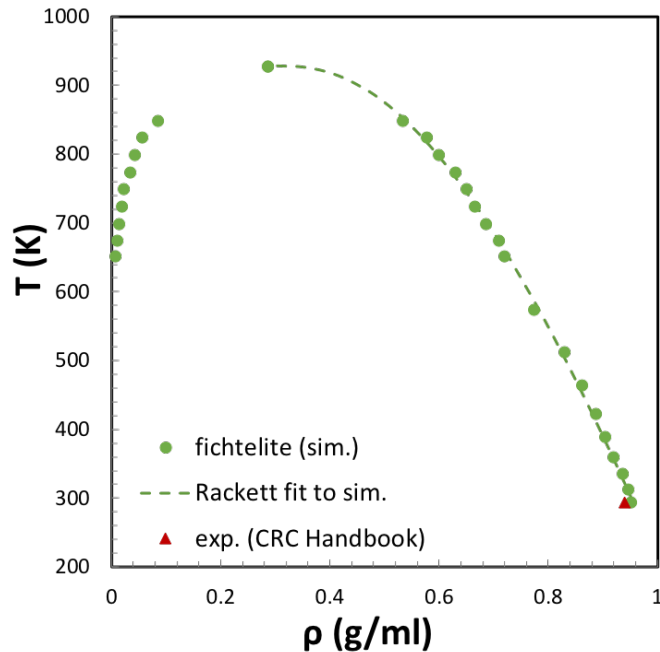
Use of correlations for
computing properties of oil
samples (multi-component)

Vapor Liquid Equilibrium (VLE) of pure compounds

Fichtelite



| T_C (K) | ρ_c (g/ml) | P_C (bar) | T_b (K) | ω |
|-----------|-----------------|-------------|-----------|----------|
| 928 | 0.285 | 21.6 | 644 | 0.291 |

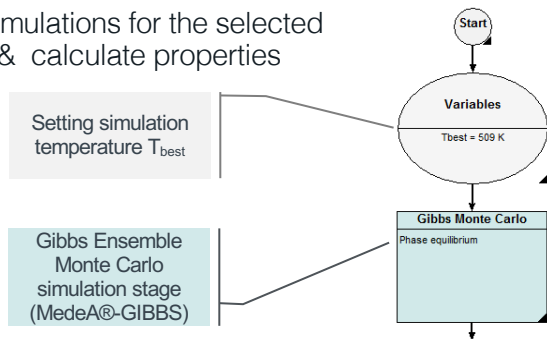


Fitting equations for pure compounds (**density**)

1 Select representative members of a chemical family

| | Increasing aromaticity, decreasing H/C, increasing liquid density | | |
|------------------|---|---|---|
| Number of cycles | Cycloalkanes (naphthenes) H/C = 1.75 to 1.85 | Naphthenoaromatics and polyaromatics H/C = 1.0 to 1.4 | Thiophenic aromatics H/C = 1.0 to 1.1 |
| 2 | 1-methyldecalin [a] C11H20 | 2,7-Dipentyl naphthalene C20H28 1,8-Dimethyltetralin [a] C12H16 | Ethyl benzothiophene [a] C10H10S |
| 3 | Fichtelite [a] C19H34 | Dimethyl octahydrophenanthrene [a] C16H22 | Retene C18H18 [a] Methyl tetrahydro dibenzothiophene [a] C13H14S |
| 4-5 | 5-alpha cholestane [a] C27H48 | Naphthenoaromatic 2A3N C23H28 [b] | Trimethyl tetrahydropicene C25H24 [a] Dimethyl Cyclohex-dibenzothiophene [a] C18H18S |

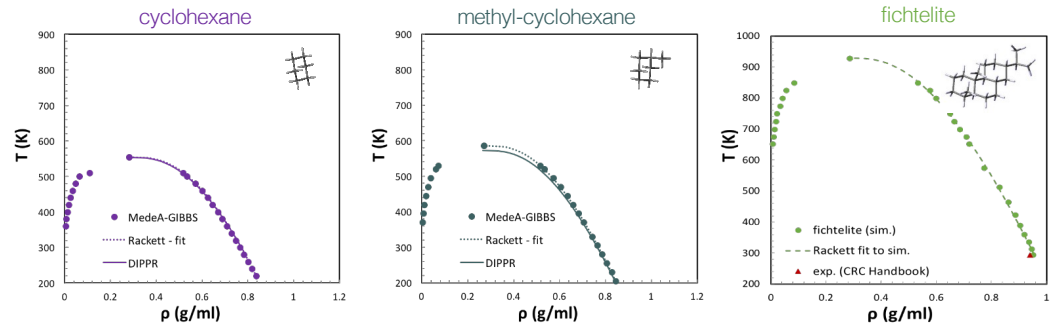
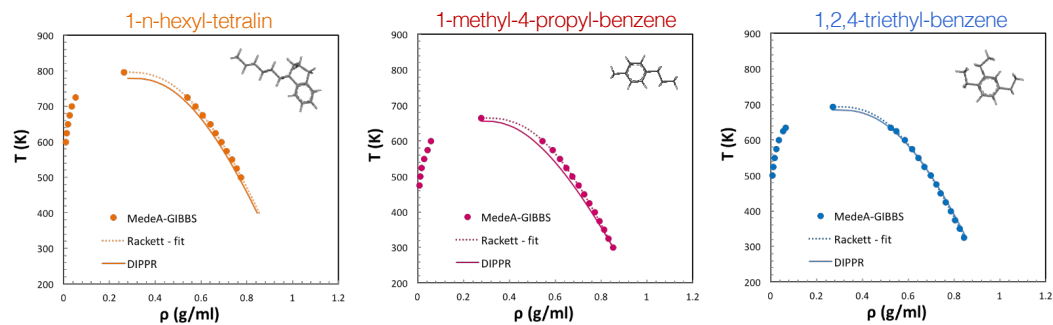
2 Run MC simulations for the selected members & calculate properties



3 Fit engineering equations on calculated properties (compound specific)

e.g. Rackett Eq.:
$$V^{sat} = V_c Z_c (1 - T_r)^A$$

Yiannourakou et al., FPE 481, p. 28-43 (2019)



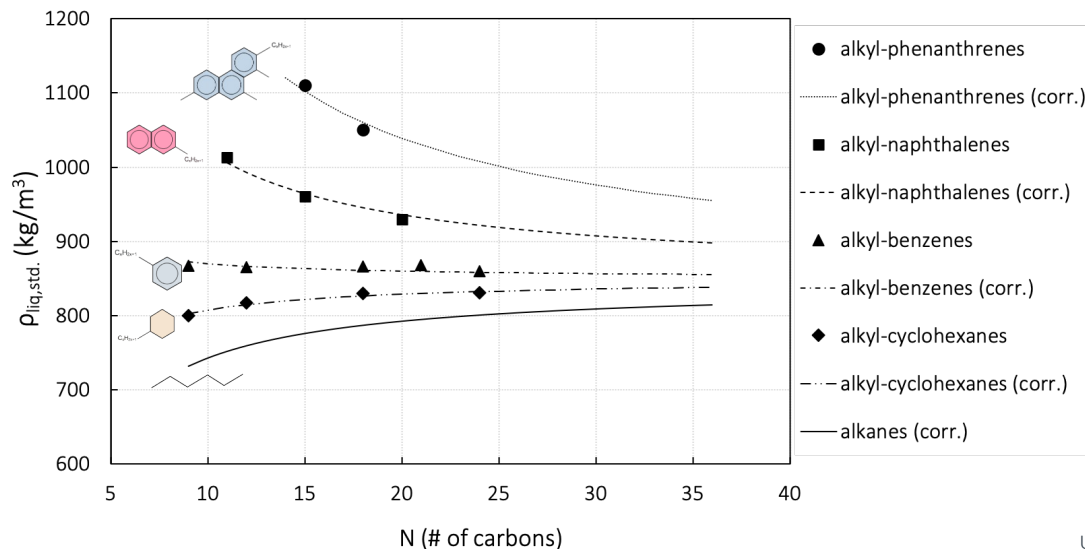
Correlations for fitting equations (pure compounds - density)

4 Create correlations for parameters of engineering equations (family specific)

e.g. Correlations for Z_C and A parameters of the Rackett equation for a specific family with the number of C atoms (N_C)

$$Z_C = a \cdot N_C^b \quad A = a \cdot N_C^2 + b \cdot N_C + c$$

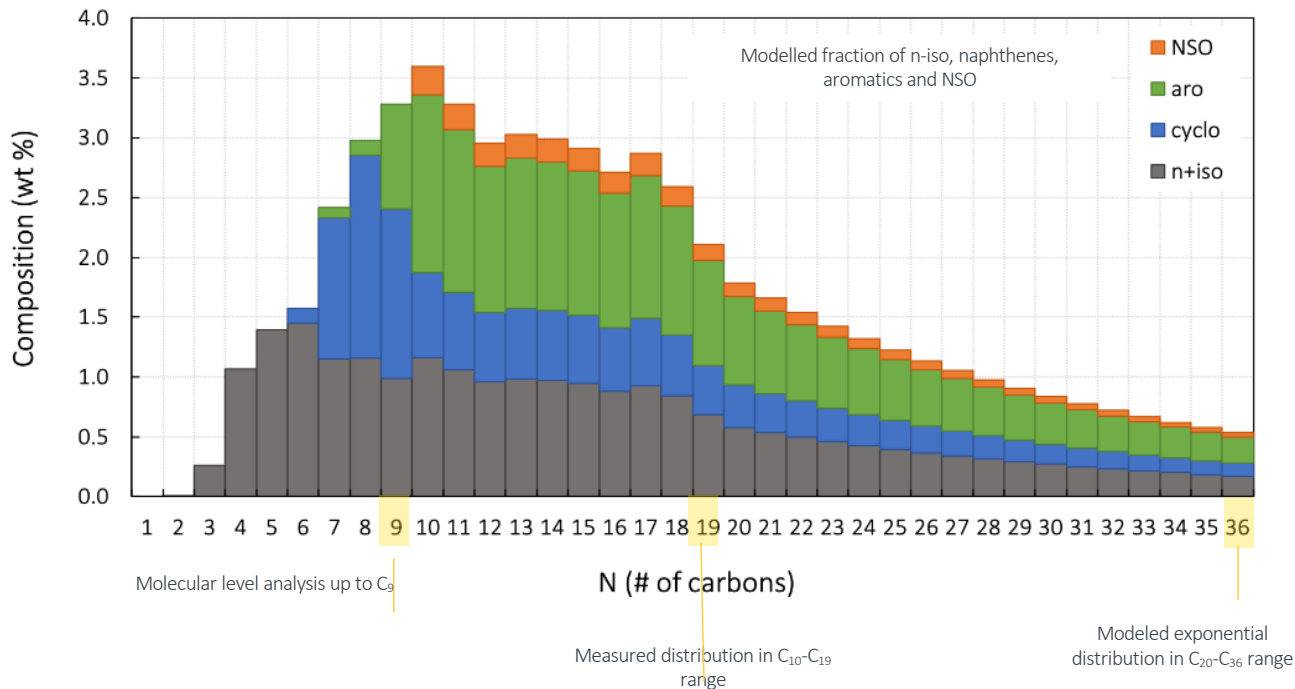
5 Use correlations to predict properties for other members of a chemical family



Ungerer et al., Energy Fuels 33, 2967-2980 (2019)

Properties of mixtures with continuous distribution of composition, from pure compound properties

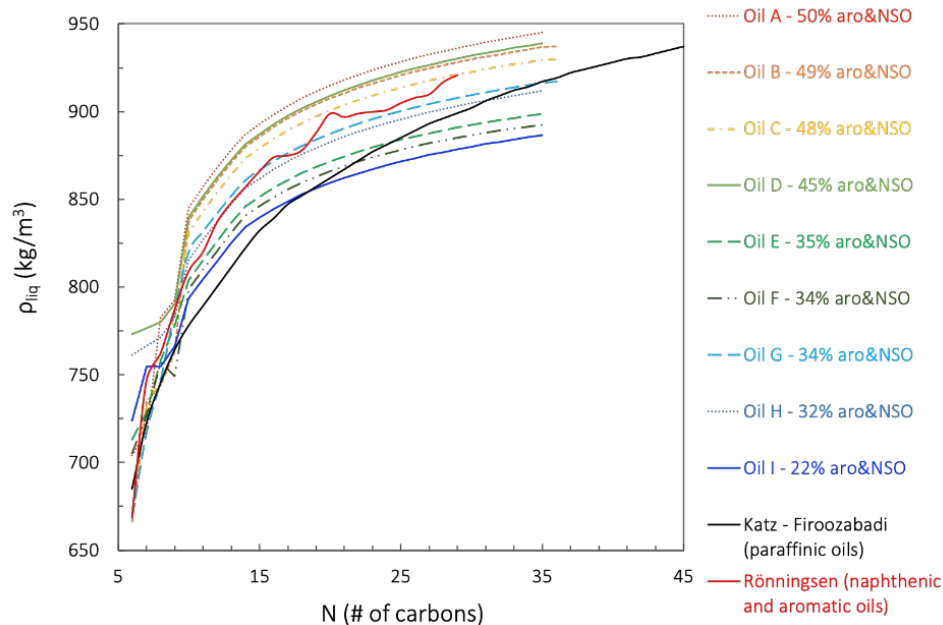
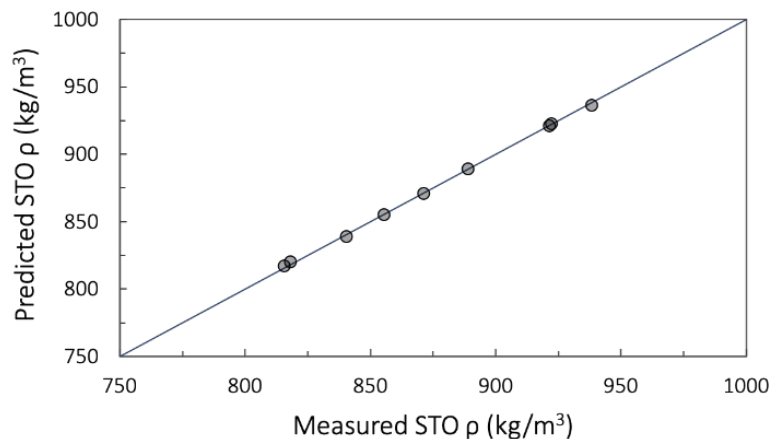
6 Use existing experimental information to create models of the mixtures (e.g. Stock Tank Oil)



Ungerer et al., Energy Fuels 33, 2967-2980 (2019)

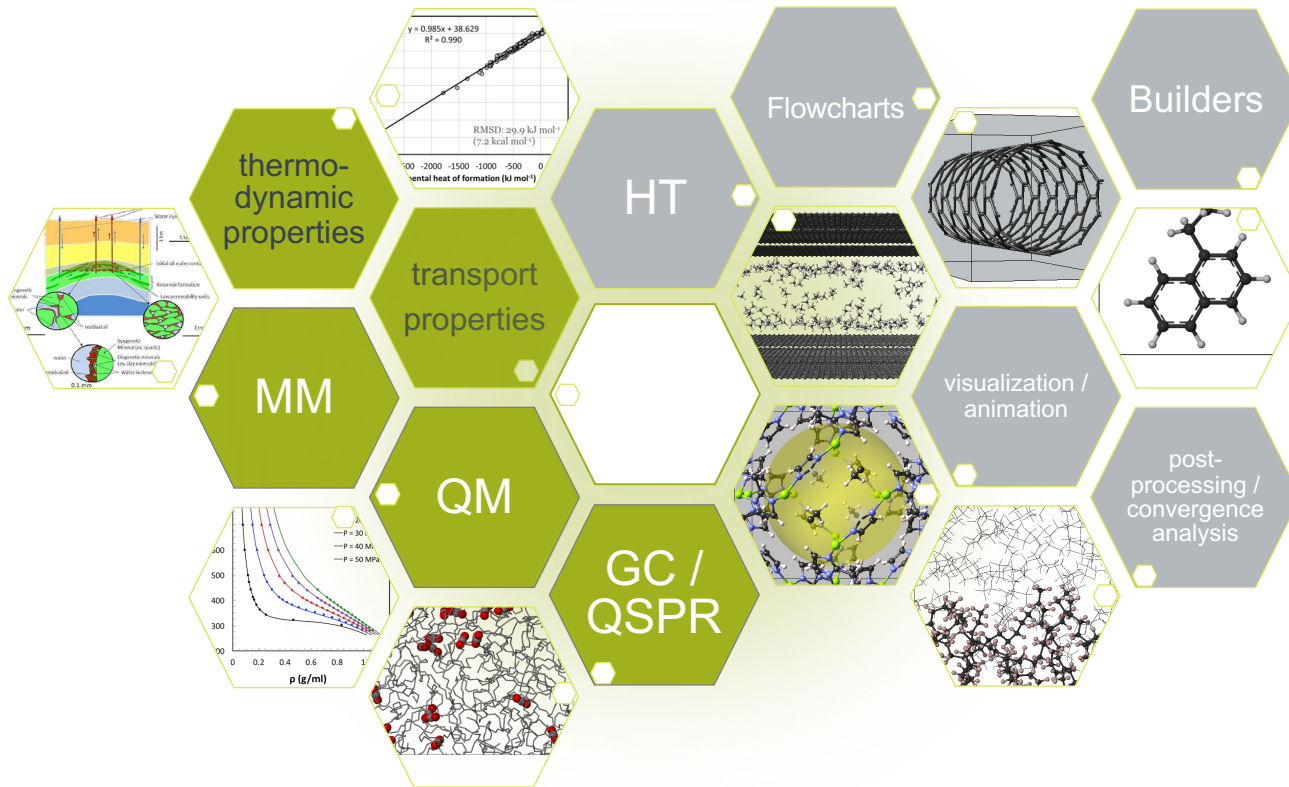
Properties of mixtures with continuous distribution of composition, from pure compound properties

7 Calculate Mixture properties, from pure compound data, e.g. density of STO (Stock Tank Oil)



Ungerer et al., Energy Fuels 33, 2967-2980 (2019)

Conclusions – Perspectives



Conclusions – Perspectives



Direct simulations can be employed for computing fluid mixtures' properties such as: VLE, diffusivity, viscosity, surface tension, etc



Depending on the property of interest and method, different accuracies may be achieved. Expected accuracies can be estimated



The use of robust workflows with automated post-processing and HT capabilities is increasing substantially the efficiency of molecular modeling

Conclusions – Perspectives



PCFF+ (AA) forcefield achieves very high coverage of organic (and some inorganic) compounds, while demonstrating also high accuracy; these forcefields are particularly useful for MD simulations



Extending UA and CG forcefields to reach higher coverage is meaningful to be able to treat many families of (organic) compounds; these forcefields are very useful particularly for MC simulations to study VLE



New forcefield types, such as Machine Learned forcefields (MLPs), may be quite interesting to explore, particularly when reactions are occurring

Conclusions – Perspectives



Consistent prediction of properties of pure compounds is achieved, from molecular simulation; these data may also be used as pseudo-experimental data



Creation of correlations for estimation of properties of pure compounds is feasible, based on molecular simulation results



Use of pure compound properties and available experimental data to optimize composition and predict properties of multi-component mixtures (e.g. oil) is feasible



Use of simulation results not only for property prediction but also for understanding the influence of phenomena that occur at the nanoscale on the macroscopic properties of a system is highly valuable

Computational effort

| Property | Property Symbol | Method used | Computational time estimate |
|--|--|------------------------------|------------------------------------|
| Vapor Liquid Equilibrium (VLE) <ul style="list-style-type: none"> Density Saturation Pressure Vaporization Enthalpy | $\rho(T)$ $P_{\text{sat}}(T)$ $\Delta H_{\text{vap}}(T)$ | MM (Monte Carlo) | hours/couple of days on 4-12 cores |
| Henry Solubility Constant | $k_{\text{H}}(P,T)$ | MM (Monte Carlo) | hours/couple of days on 4-12 cores |
| Solubility | | MM (Monte Carlo) | hours/couple of days on 4-12 cores |
| Viscosity | $\eta(P,T)$ | MM (molecular dynamics) | hours/days on 16-32 cores |
| Diffusivity | $D(P,T)$ | MM (molecular dynamics) | hours/days on 16-32 cores |
| Thermal Conductivity | $\lambda(P,T)$ | MM (molecular dynamics) | hours/days on 16-32 cores |
| Surface Tension | $\gamma(P,T)$ | MM (molecular dynamics) | days on 16-32 cores |
| Reaction Kinetics | $\Delta G^{\#}(T)$, $k(T)$, $r(T)$ | QM & MM (molecular dynamics) | hours/days on 16-32 cores |

MM: molecular mechanics, QM: quantum mechanics, FF: ForceField

Credits

- **LAMMPS:**

- S. Plimpton, *Fast Parallel Algorithms for Short-Range Molecular Dynamics*, J Comp Phys, 117, 1-19 (1995), www.lammps.sandia.gov
- A. P. Thompson, H. M. Aktulga, R. Berger, D. S. Bolintineanu, W. M. Brown, P. S. Crozier, P. J. in 't Veld, A. Kohlmeyer, S. G. Moore, T. D. Nguyen, R. Shan, M. J. Stevens, J. Tranchida, C. Trott, S. J. Plimpton, *LAMMPS - a flexible simulation tool for particle-based materials modeling at the atomic, meso, and continuum scales*, Comp. Phys. Comm. 271, p. 10817 (2022).

- **GIBBS:** License IFP-EN – LCP (CNRS – Université Paris Sud)

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- E. Bourasseau, M. Haboudou, A. Boutin, A.H. Fuchs, P Ungerer, The Journal of chemical physics 118 (7), 3020-3034
- A.D. Mackie, .B Tavitian, A. Boutin, A.H. Fuchs, Molecular Simulation 19 (1), 1-15
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MedeA Modules Used

MedeA Environment: Materials Modeling and Simulation Environment

MedeA Molecular Builder: Create 3D molecular models. Import and edit molecular systems or build them stepwise using the MedeA molecular fragment library.

MedeA Amorphous Materials Builder: Create condensed phase models based on system chemical composition and target density. It eliminates lengthy mixing and amorphization simulations through realistic sampling of the translational, rotational, and conformational degrees of freedom of component species.

MedeA GIBBS: MedeA GIBBS focuses on the prediction of fluid properties in various equilibrium conditions such as molecular liquids of complex structure, sorption in natural and industrial adsorbents, solubility of small compounds in polymer materials, and ion exchange.

MedeA LAMMPS: MedeA LAMMPS focuses on the efficient execution of computational tasks using computational hardware ranging from massively parallel facilities to laboratory-scale workstations and gpu-enabled clusters.

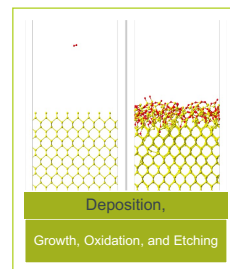
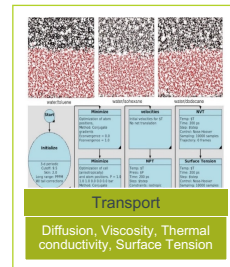
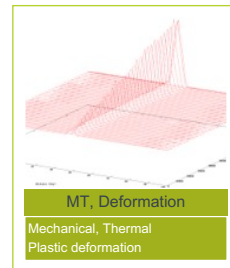
MedeA Modules Used

MedeA Thermal Conductivity: Calculate lattice thermal conductivity with Green-Kubo or non-equilibrium MD Müller-Plathe

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Questions about Materials Design Webinars

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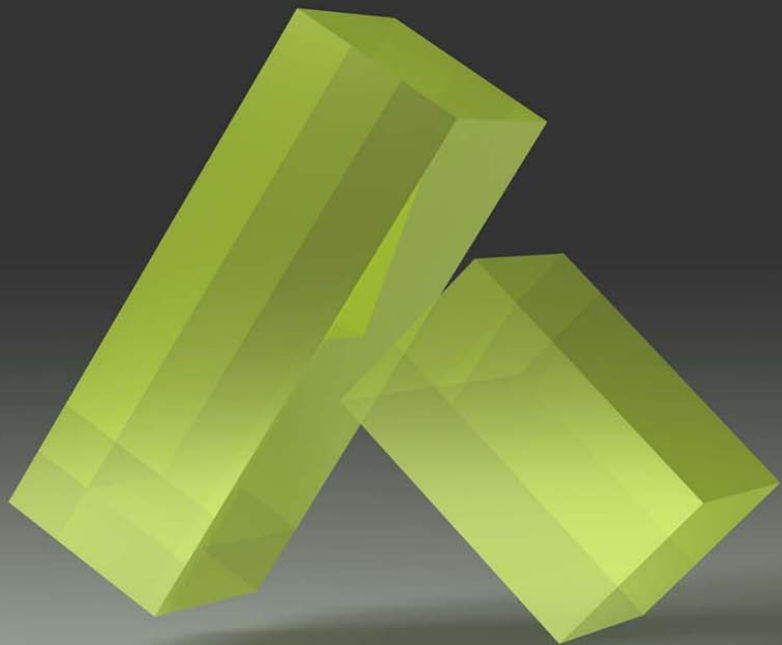
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