



Materials Design

2024 UGM Webinar Series

Mechanistic and Structural Sources of Complexity in the Atomic Scale Simulation of Brønsted Acidic Zeolite Catalysts

Dr. Céline Chizallet

IFP Energies nouvelles

October 15, 2024





Materials Design UGM

UGM 2024

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*Tuesdays and Thursdays
October 15 – November 7*

Plenary Speakers:

Professor Sir Richard Catlow - University College London, England

***Professor Georg Kresse, Dr. Martijn Marsman,
and Dr. Manuel Engel - The University of Vienna, Austria***

Professor Greg Olson - Massachusetts Institute of Technology, USA

Dr. Céline Chizallet - IFP Energies Nouvelles, France

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Materials Design UGM Presenter



Dr. Céline Chizallet

Project leader

Catalysis, Biocatalysis and Separation Division

IFP Energies nouvelles, France



Webinar Speakers

Katherine Hollingsworth

khollingsworth@materialsdesign.com

Dr. Alexander Mavromaras

amavromaras@materialsdesign.com

Materials Design UGM Webinar Series

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- We will be recording this session

- Upcoming sessions are posted on the UGM site

- Watch any of our earlier webinars anytime www.materialsdesign.com/webinars

- Brief survey

- Take a 2 minutes brief survey at the end of the webinar

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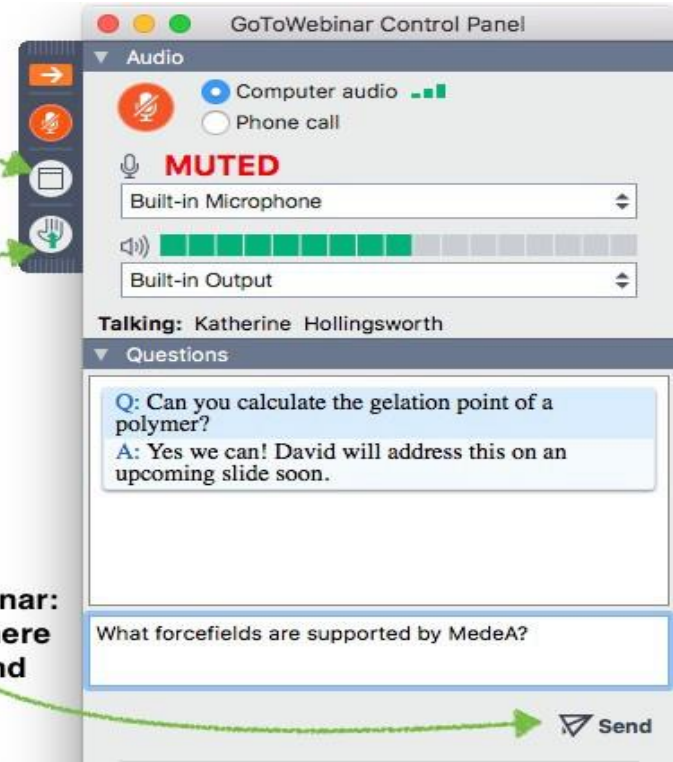
Please Ask Questions!

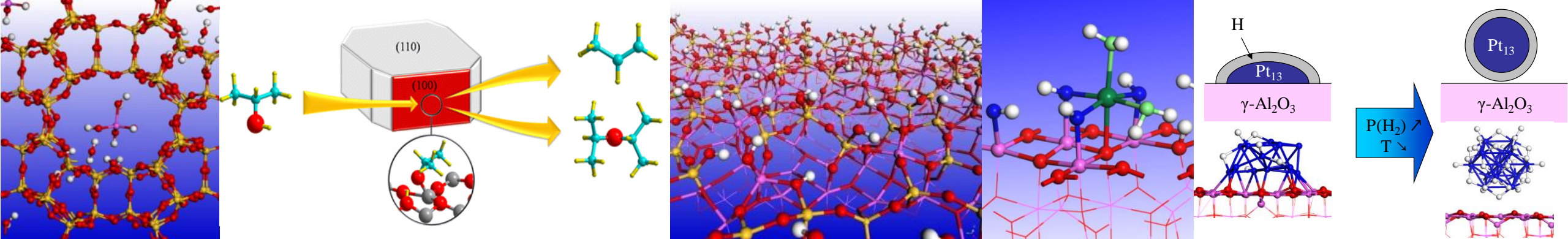
full screen

during discussion:
raise hand
to speak

Use the raise hand icon to bring
attention to your question

any time during webinar:
type your question here
and then press Send





MECHANISTIC AND STRUCTURAL SOURCES OF COMPLEXITY IN THE ATOMIC SCALE SIMULATION OF BRØNSTED ACIDIC ZEOLITE CATALYSTS

CELINE CHIZALLET

IFP Energies nouvelles
Catalysis, Biocatalysis and Separation Division
Rond Point de l'échangeur de Solaize, BP3
69360 Solaize, FRANCE

celine.chizallet@ifpen.fr

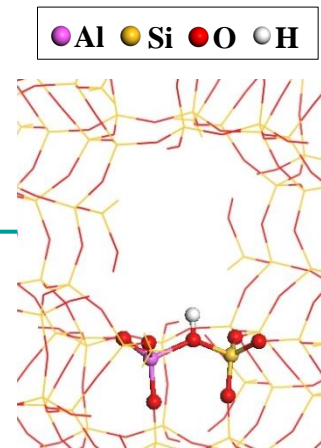


BRØNSTED ACIDIC ZEOLITE CATALYSTS

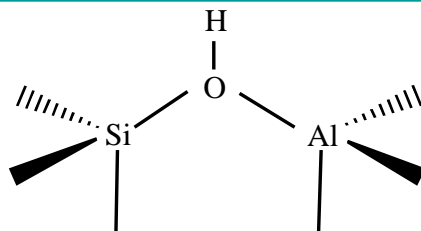
* Practical relevance of proton exchanged zeolites in catalysis

- Refining, petrochemistry, biomass conversion, plastic recycling
- Cationic or cationic-like intermediates invoked (carbenium/carbonium chemistry)
- Mechanisms still questioned

Molecular Views on Mechanisms of Brønsted Acid-Catalyzed Reactions in Zeolites
C. Chizallet, C. Bouchy, K. Larmier, G. Pirngruber, *Chem. Rev.*, 2023, 123, 6107



* Bulk sites in micropores



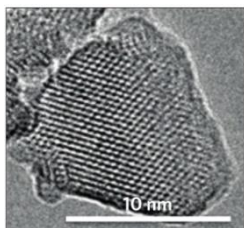
Uytterhoeven, Christner, Hall, *JPC* 1965

Haag, Lago, Weisz, *Nature* 1984

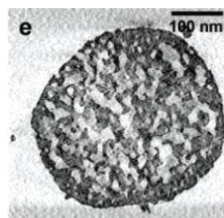
Mortier, Sauer, Lercher, Noller, *JPC* 1984

* Beyond the crystal bulk approach

- External surface / surface at mesopores

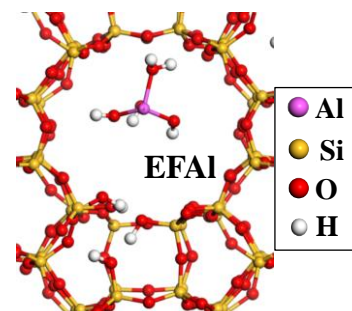


Nano-FAU, Mintova et al.
Nature Materials 2015

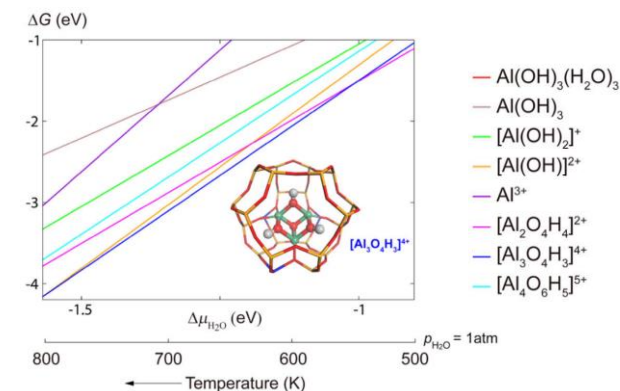


Hierarchical-MFI, Perez-Ramirez et al.
JACS 2005

- Defects, EFAIs



J. Catal. **2016**, 339, 242



Pidko et al. *ACS Catal.* **2015**, 5, 7024

Need for molecular approaches

C. Chizallet, *ACS Catal.* 2020, 10, 5579–5601

FROM RATIONALIZATION TO PREDICTION OF COMPLEX CATALYTIC SYSTEMS

I- Structure understanding

- **Model** construction for active sites
- Electronic and stability analysis
- Comparison with experimental **spectral feature**



II- Chemical reactivity investigations

- Adsorption of **reactants**
- Determination of **intermediates** and **transition structures**
- Calculation of **free energy profiles and** full reaction **pathways**



III- Towards prediction

Multiscale modeling : prediction of macroscopic **activity / selectivity**

Quantum chemistry approach:

$$H\Psi = \varepsilon\Psi$$

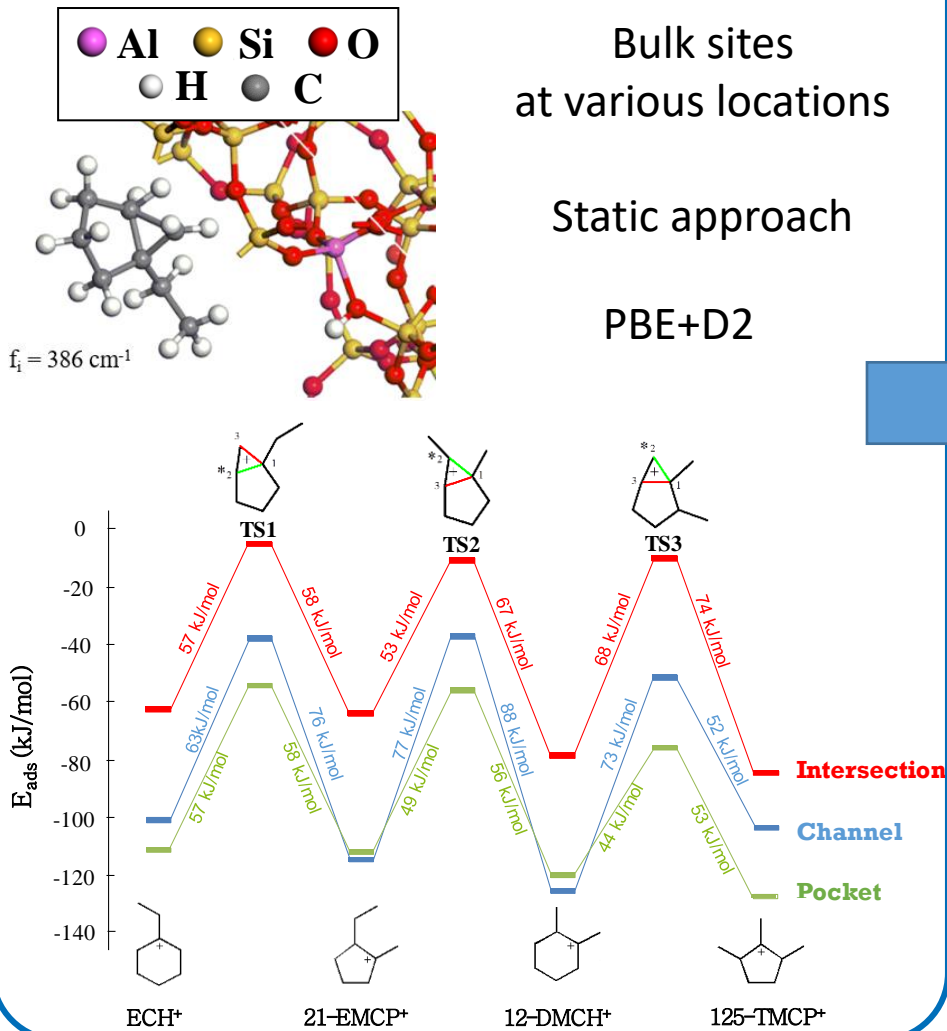


$$k = \frac{k_B T}{h} \exp\left(-\frac{\Delta_r H^\ddagger - T\Delta_r S^\ddagger}{RT}\right)$$

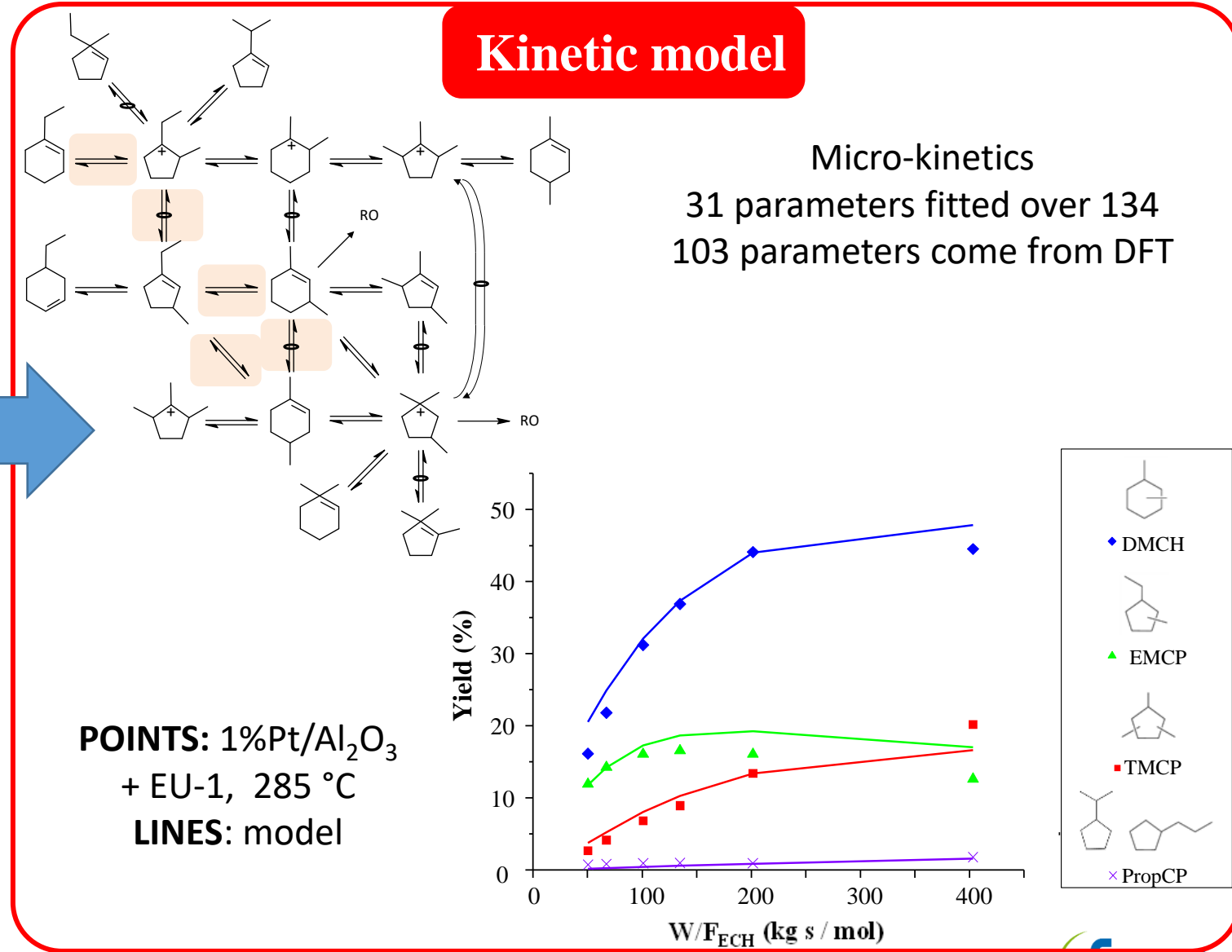
Rate of elementary step =
- $d[R]/dt = k [R]$

A SUCCESSFUL EXAMPLE WITH "LOW EFFORT": BIFUNCTIONAL HYDROISOMERIZATION OF ETHYL-CYCLOHEXANE IN EU-1

DFT calculations



Kinetic model



SAMPLING PROBLEMS WITH THE STATIC APPROACH

Carbenium chemistry in Brønsted acid zeolites :
variety of local minima and saddle points

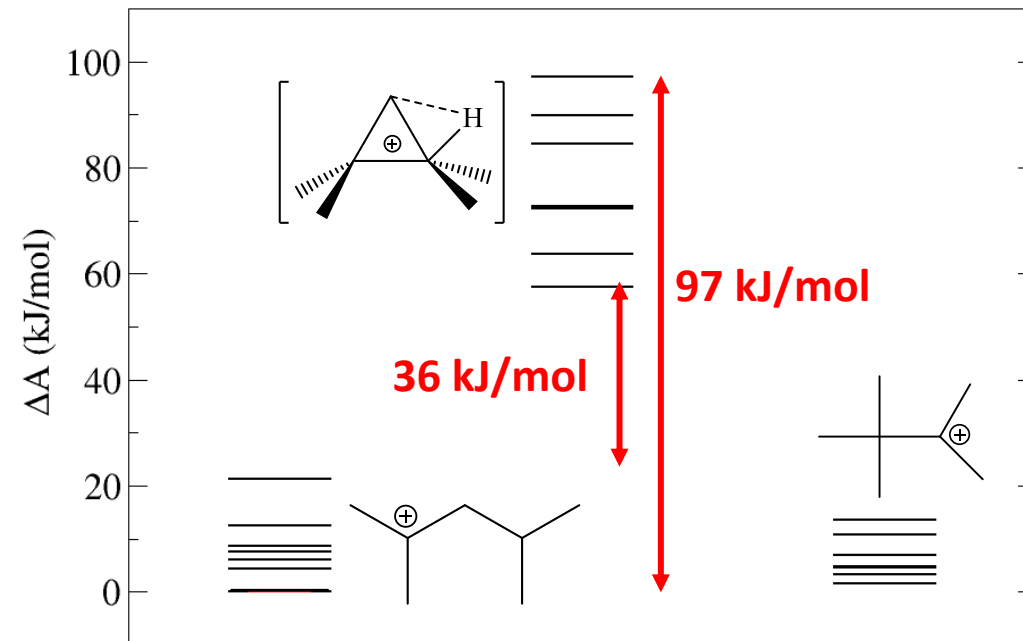
Deviation of ~60 kJ/mol on barriers
→ Ratio ~ $2 \cdot 10^6$ on rate constants k at 500 K !

Typical computational
time scale ratio:

Static → AIMD
1 → **10^3-10^4**

Type B isomerization

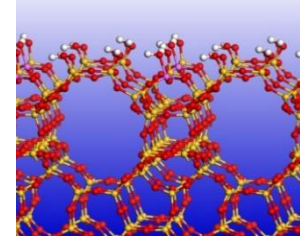
(CHA)



Rey, Gomez , Raybaud, Chizallet , Bučko, *J. Catal.*, **2019**, 373, 361

SIMULATION OF INTRICATE ZEOLITE CATALYSTS

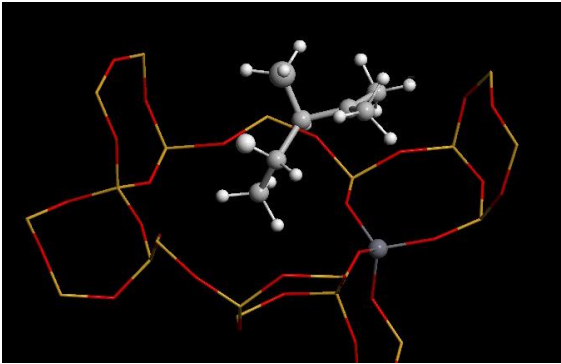
Acid sites at the external surface



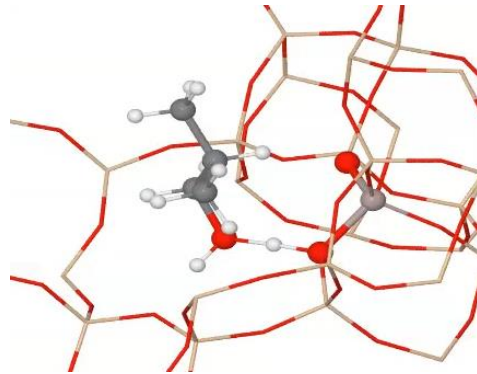
Static investigation of the reactivity of bulk sites

Structural complexity

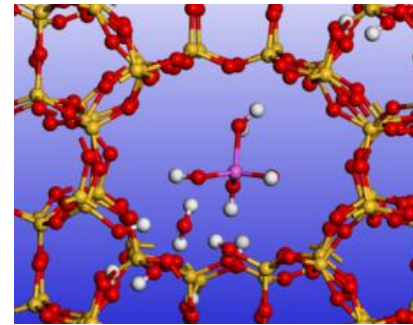
Alkene isomerisation and cracking



Alcohol dehydration



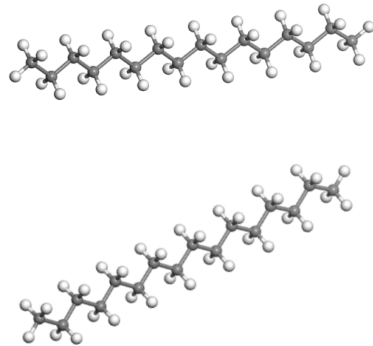
Dealumination mechanisms



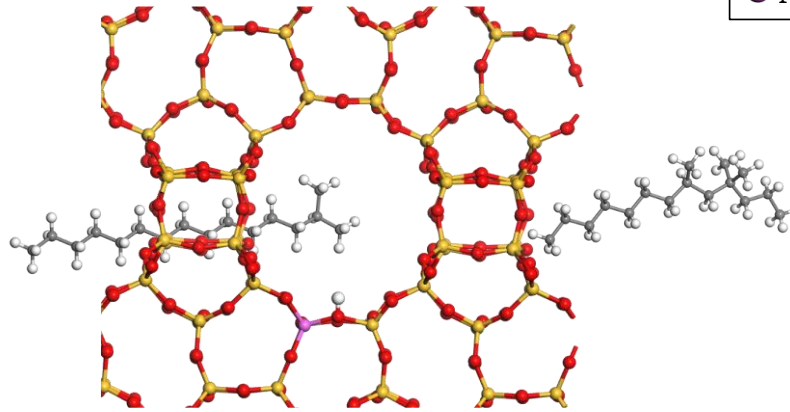
Complexity of chemical reaction investigations: AIMD

ALKANE ISOMERIZATION AND CRACKING BY PROTON EXCHANGED ZEOLITES

Heavy feedstocks



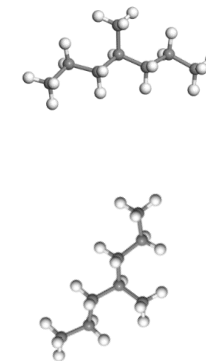
Plastic waste, vegetable oils, Fischer-Tropsch process products, crude oils...



Hydrocracking

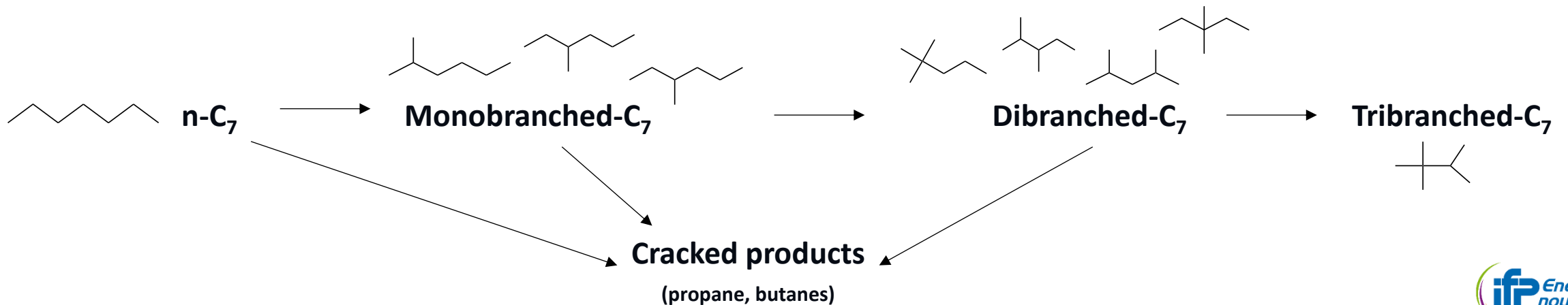


Refined products

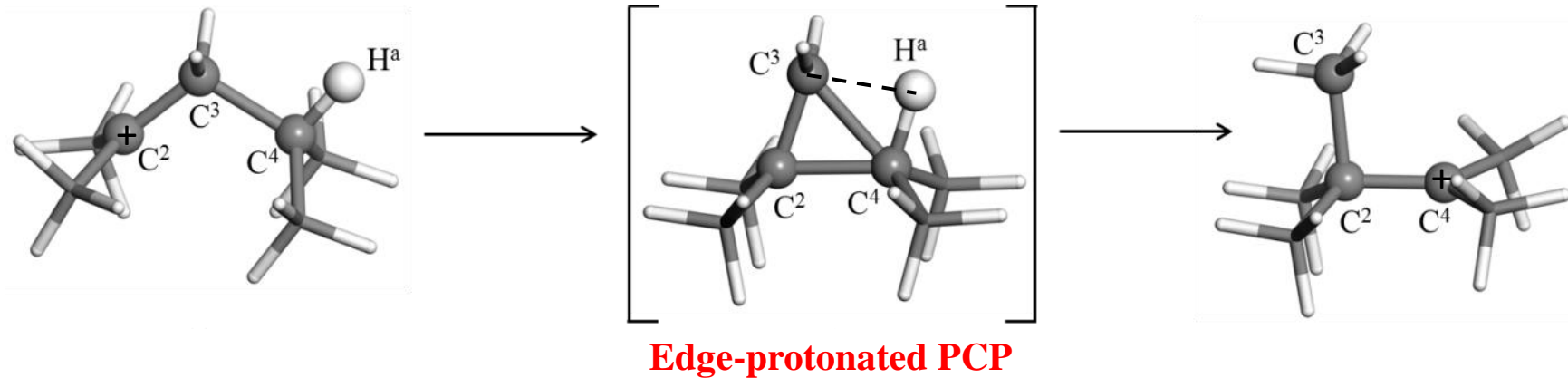
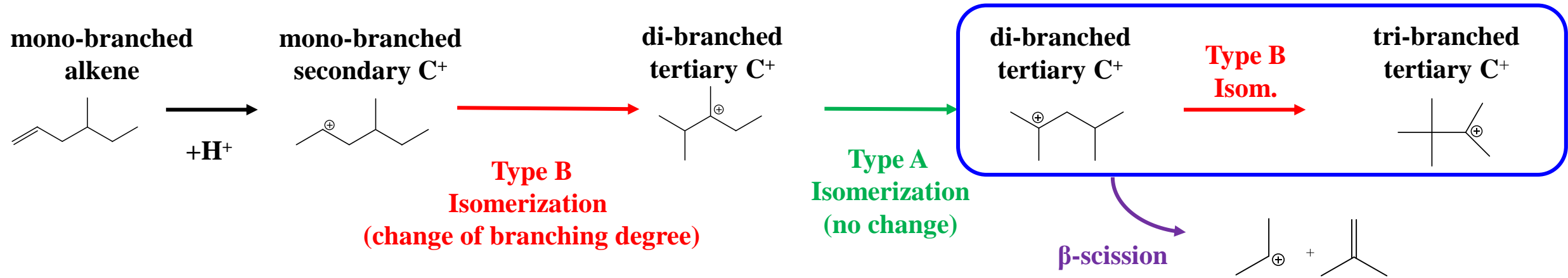


monomers, fuel

Hydroconversion of n-heptane as a model reaction:



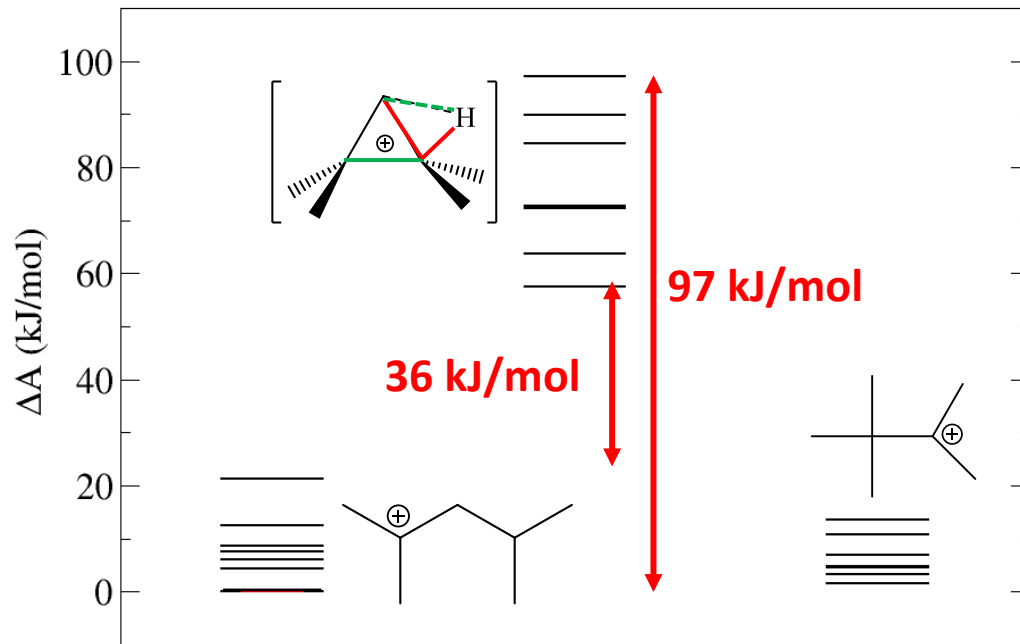
Bifunctional: alkenes as reactants in the zeolite



TYPE B ISOMERIZATION BETWEEN TWO TERTIARY CARBENIUM IONS

Static approach

Variety of local minima and saddle points

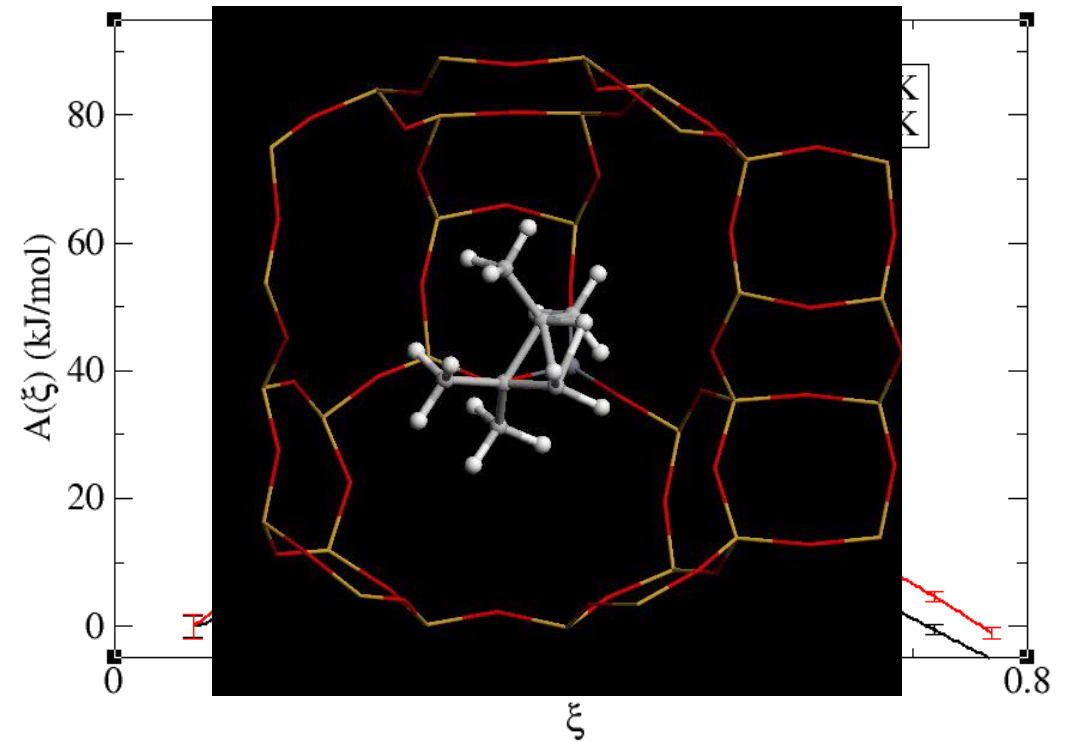


Free energies given at 300 K

PBE+D2

Ab initio molecular dynamics (AIMD)

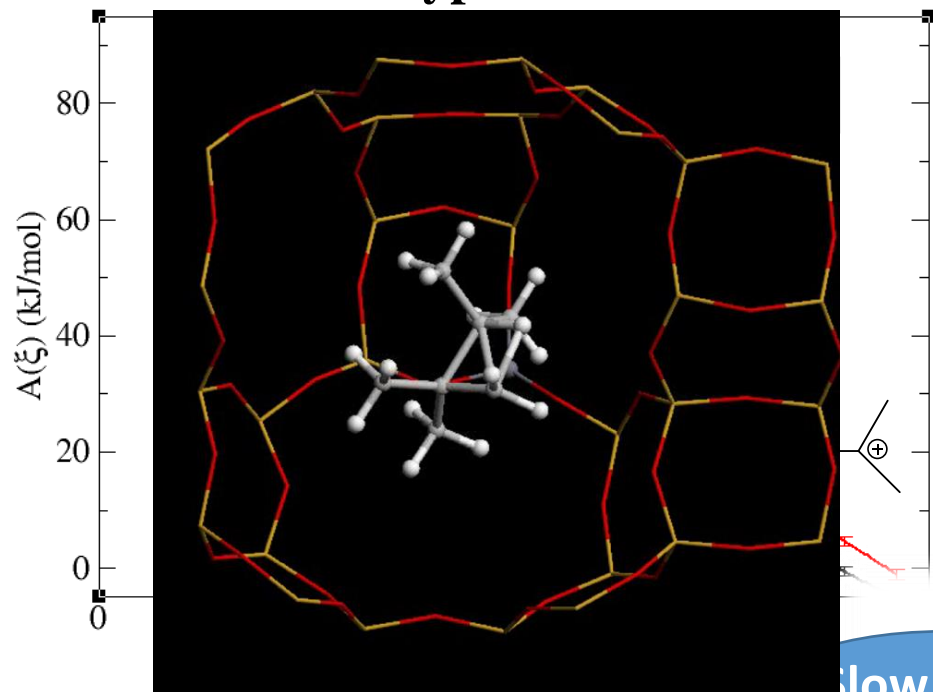
Constrained molecular dynamics (Blue Moon Sampling)



J. Rey, A. Gomez, P. Raybaud, C. Chizallet, T. Bucko, *J. Catal.*, 373, 361-373, 2019

TYPE A VERSUS TYPE B ISOMERIZATION

Type B

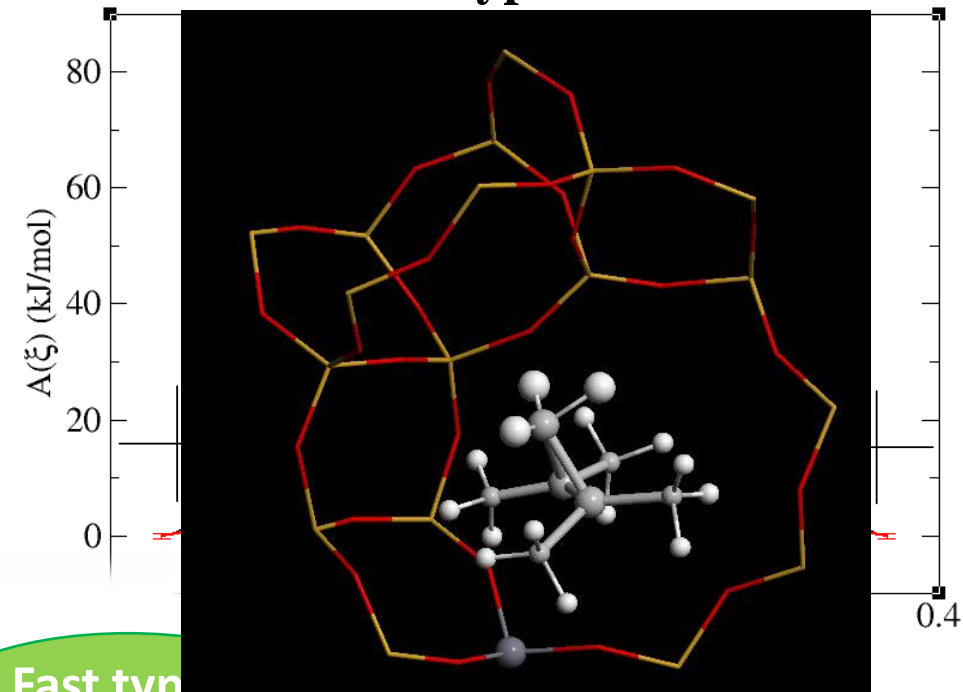


Tight TS:
constrained C-C
and C-H bonds,
repulsion and
lower entropy

PBE+D2

Zeolite: CHA

Type A

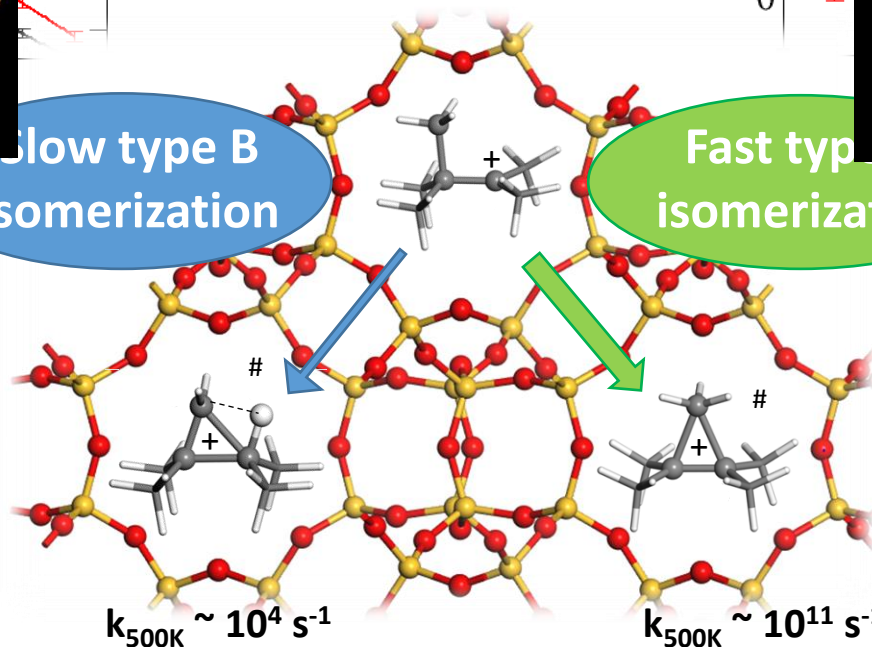


Loose TS:
longer C-C bonds and
free rotating CH₃,
lower repulsion and
higher entropy

Atomic origin of
the difference:
bridging H in
edge-protonated
PCP TS_B

Slow type B
isomerization

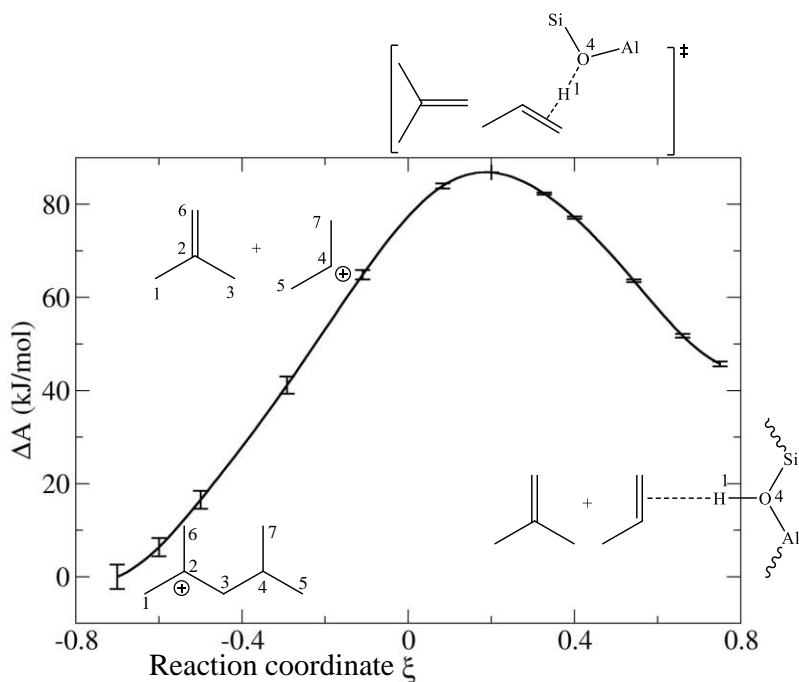
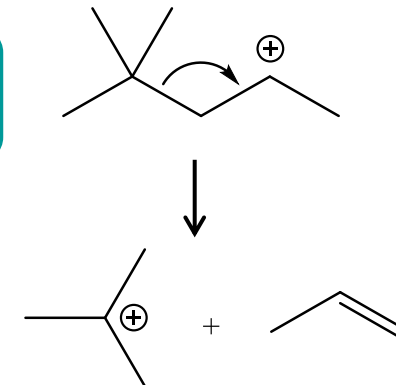
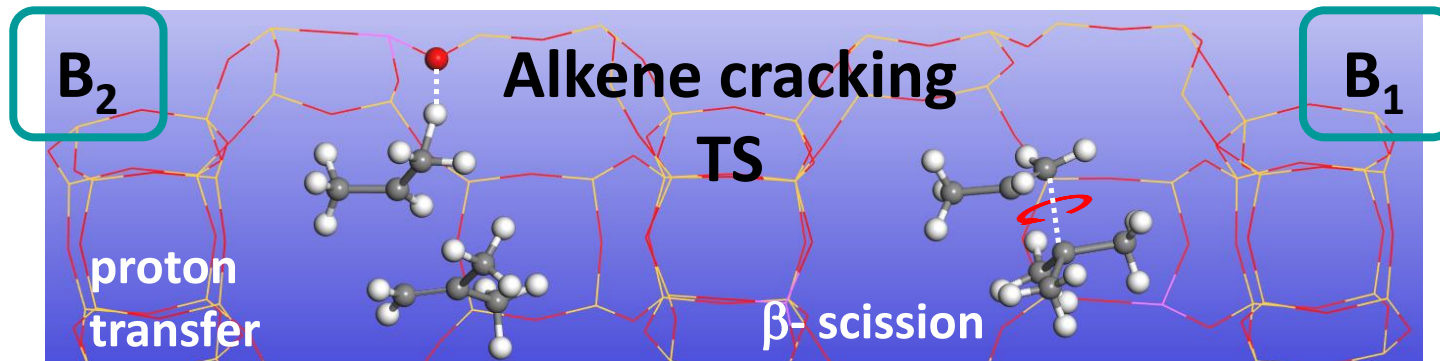
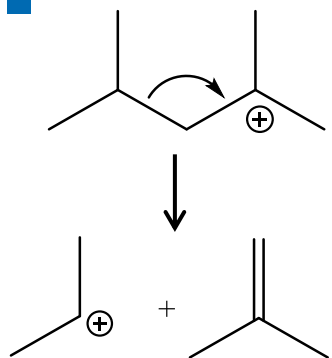
Fast type A
isomerization



J. Rey, A. Gomez, P. Raybaud, C. Chizallet,
T. Bucko, *J. Catal.*, 373, 361-373, 2019

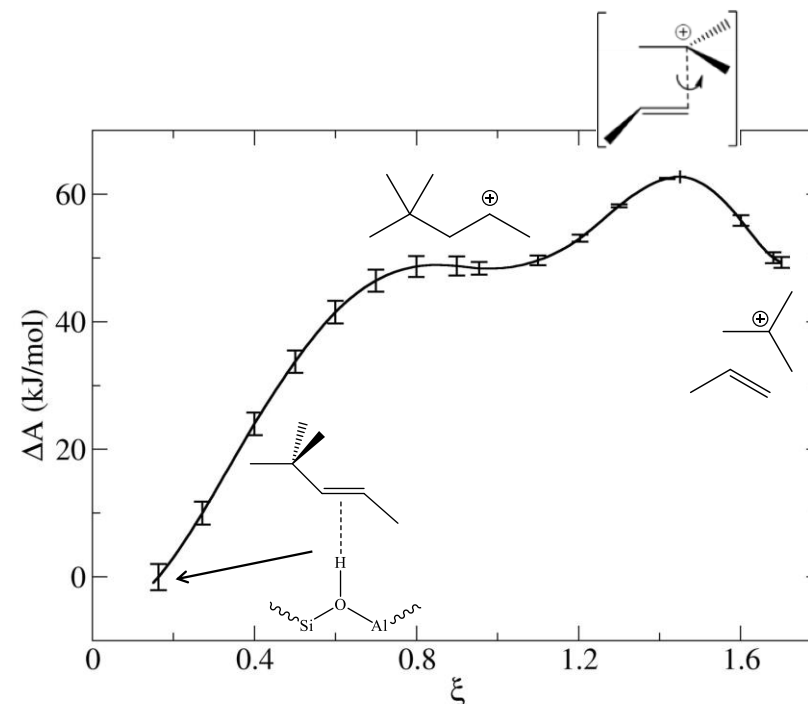
CRACKING REACTIONS

AIMD,
PBE+D2



B₂ cracking: not the usually admitted TS, secondary cation produced is not a stable intermediate

B₁ cracking:
 - not the usually admitted reactant,
 - high entropy of the β-scission TS due to dynamic effects



KINETIC MODELLING, COMPARISON WITH EXPERIMENTS

Ab initio based microkinetic model

Tabulated data for hydro-dehydrogenations of alkenes/alkanes in gas phase, equilibrium at each simulation step

Ab initio rate constants for reactions undergone by alkenes in the zeolite: adsorption, protonation, isomerization, cracking → lumping

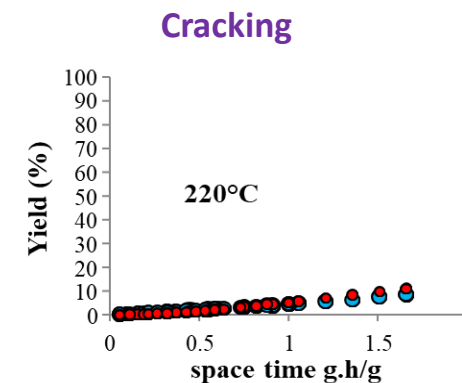
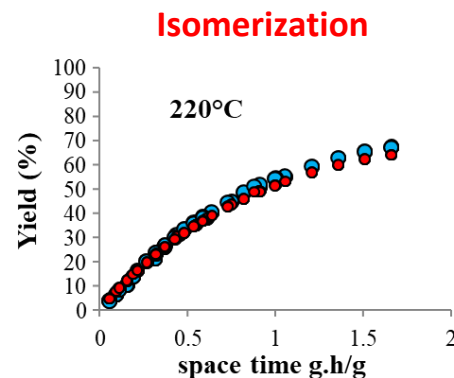
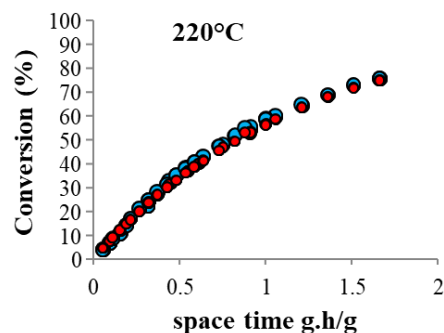
High Throughput Experiments

Catalyst: Pt/Beta (BEA)

HTE: 16 reactors, Flowrence Avantium

Kinetic study: variation of %Pt, T, P_{tot}, H₂/HC, τ

● experiments
● simulation



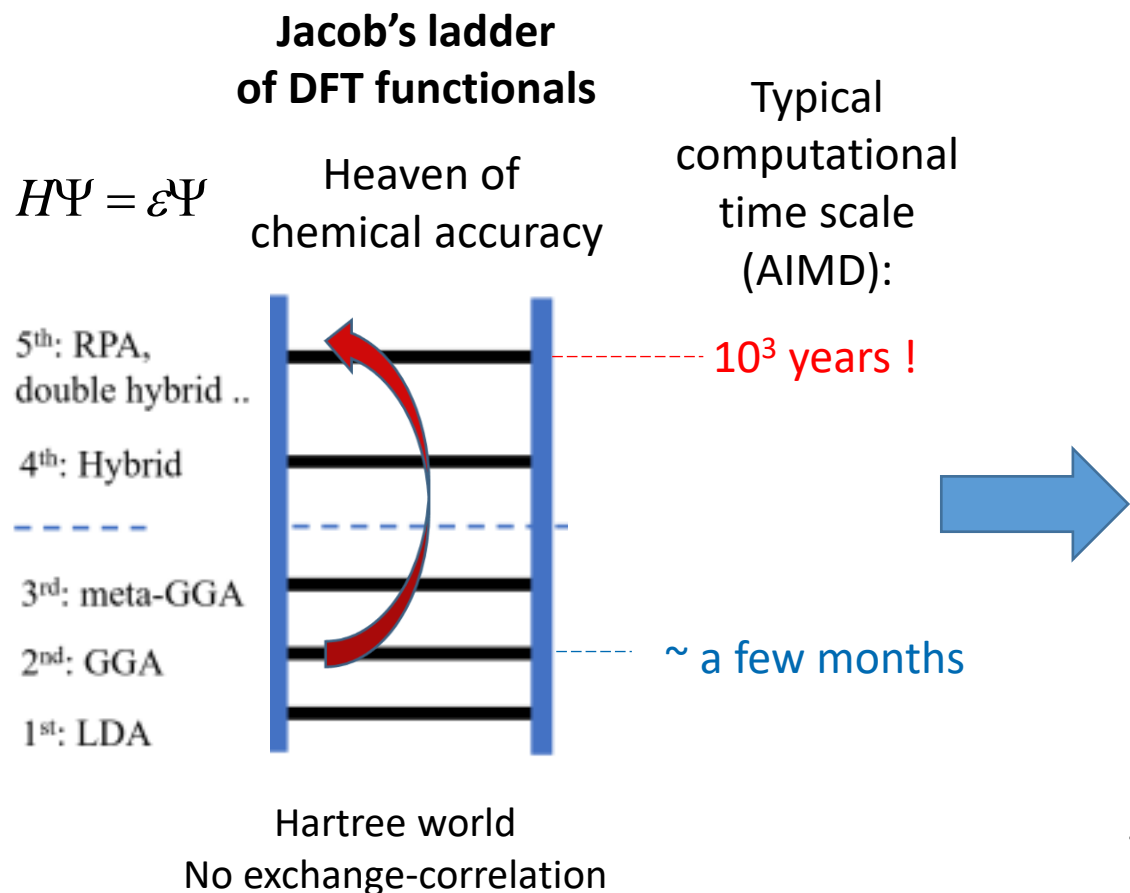
Adjustments of barriers:

data	original value	adjusted value
ΔG_{+}^{\ddagger} (type C cracking) (kJ·mol ⁻¹)	24	40
ΔG_{+}^{\ddagger} (type B1 cracking) (kJ·mol ⁻¹)	15	30
ΔG_{+}^{\ddagger} (type B2 cracking) (kJ·mol ⁻¹)	84	93

DFT underestimates by 10-15 kJ/mol the difference between the cracking barriers and the isomerization barriers

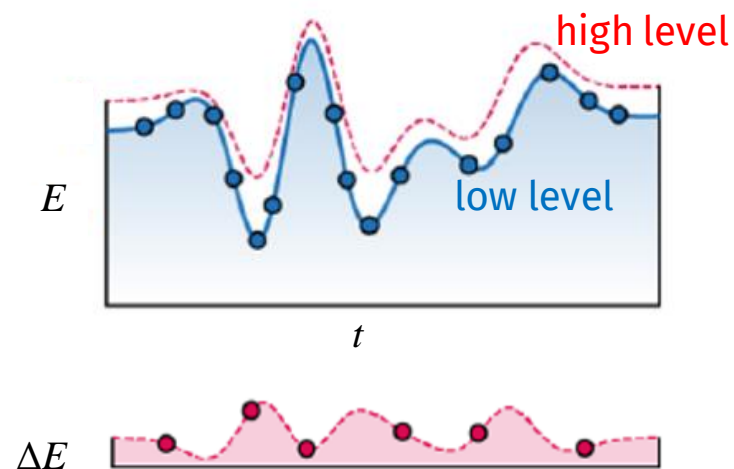
Improvements to be made: lack of accuracy of DFT ? Effect of the level of theory ?

COMPUTING FREE ENERGY BARRIERS WITH AIMD AT THE RPA LEVEL



MLPT: Machine Learning Perturbation Theory

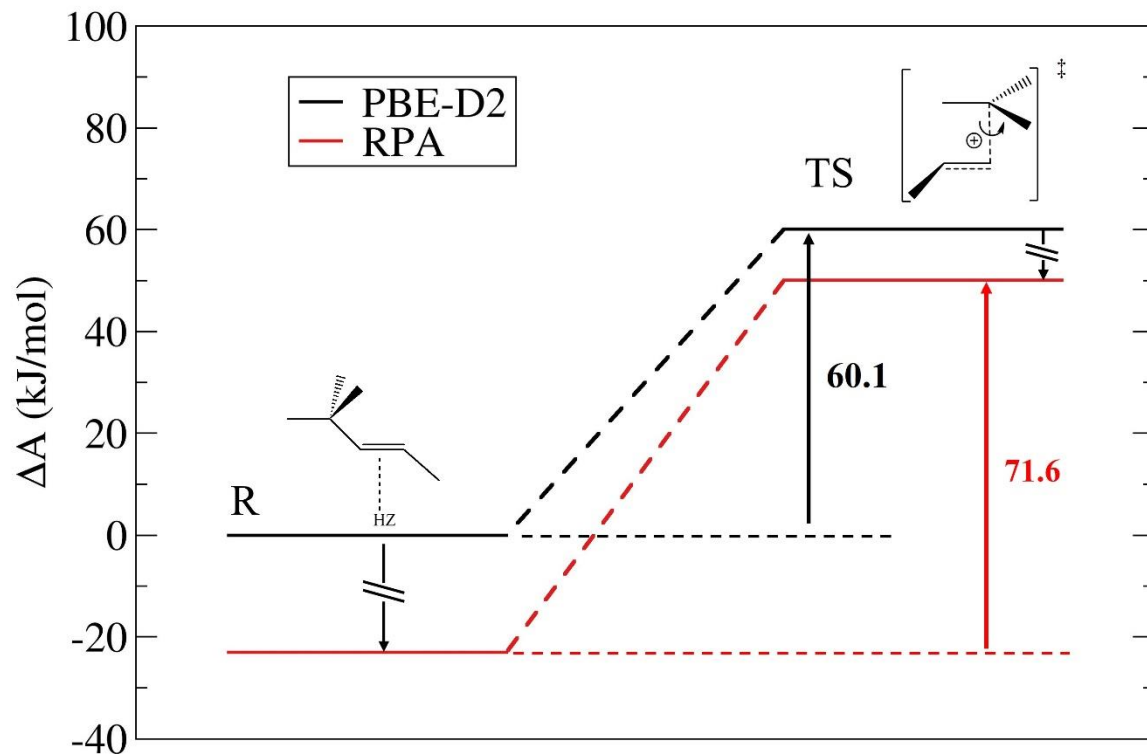
- **Step 1:** AIMD at a “low” production level (PBE+D2)
- **Step 2:** Compute only a few (~ 100) **single point energy calculations on some configurations at the high target level**



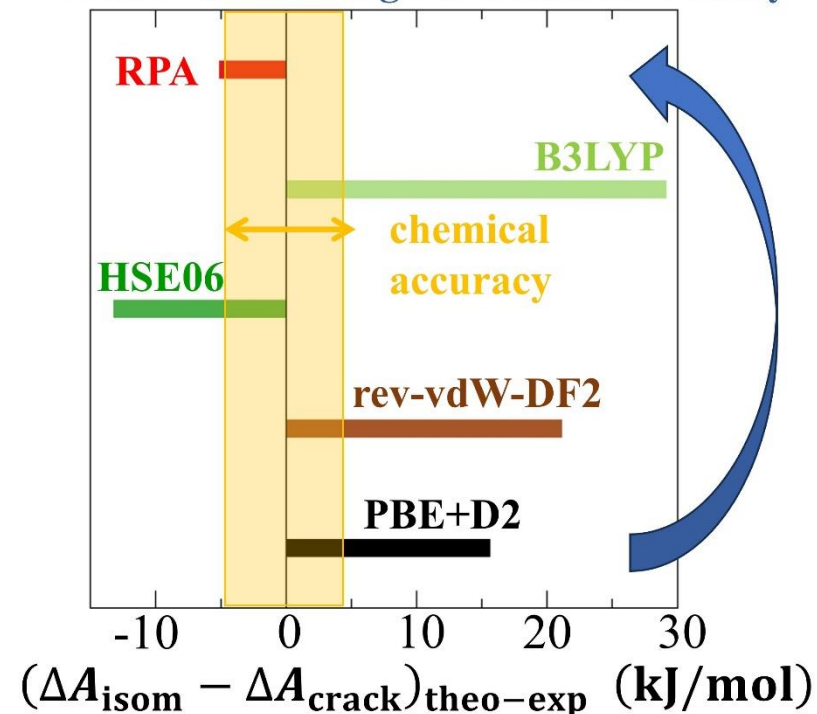
- **Step 3:** Train a **Machine Learning** model to quantify the difference in energy between the two levels thanks to **structural descriptors**
- **Step 4:** Apply **Perturbation Theory** to deduce the free energy at the high level of theory

FREE ENERGY BARRIERS OF ISOMERIZATION VERSUS CRACKING

Correction of the B₁ cracking free energy profile:



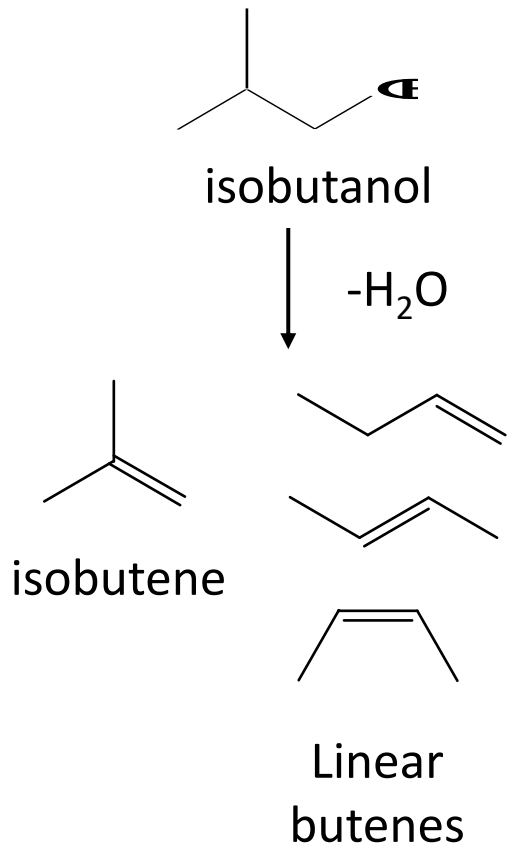
Climbing the Jacob's ladder by Machine Learning Perturbation Theory



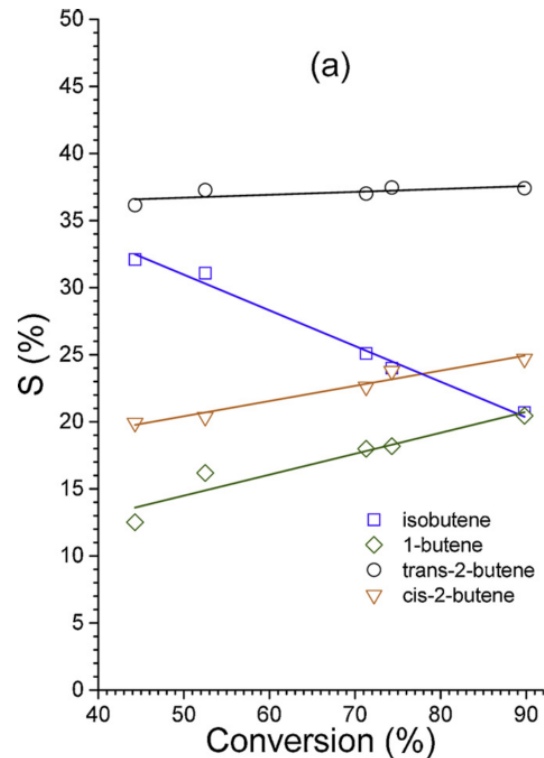
RPA-MLPT provides the best (and necessary) accuracy

Combining AIMD and RPA would not have been possible without Machine Learning Perturbation Theory

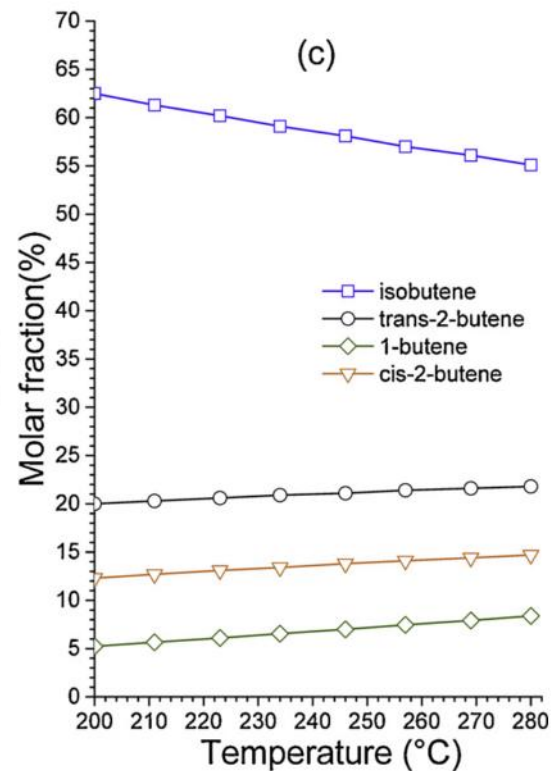
ISOBUTANOL DEHYDRATION INTO LINEAR ALKENES



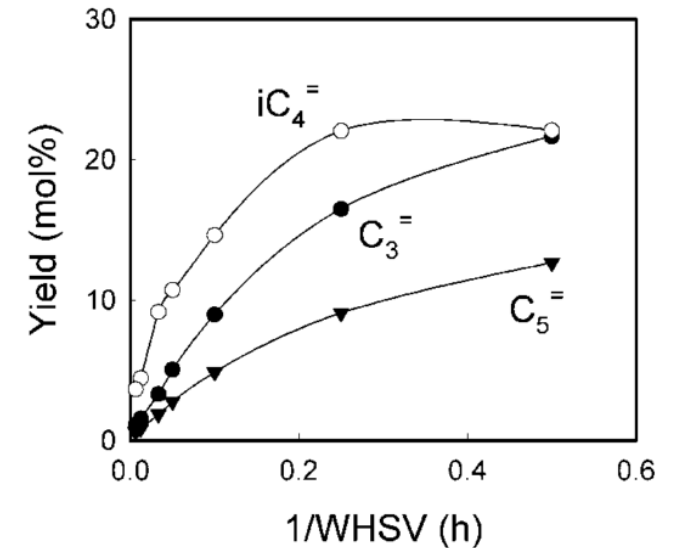
Isobutanol dehydration (250°C, ferrierite):



Equilibrium composition:



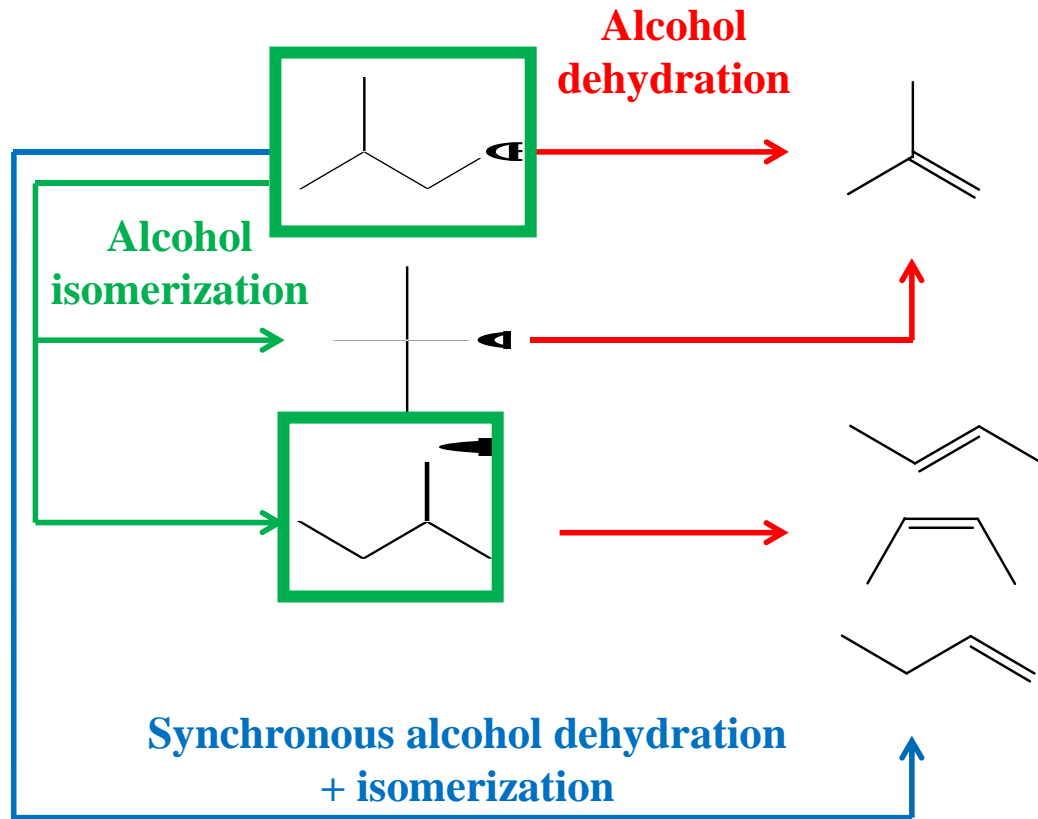
Conversion of but-1-ene (350°C):



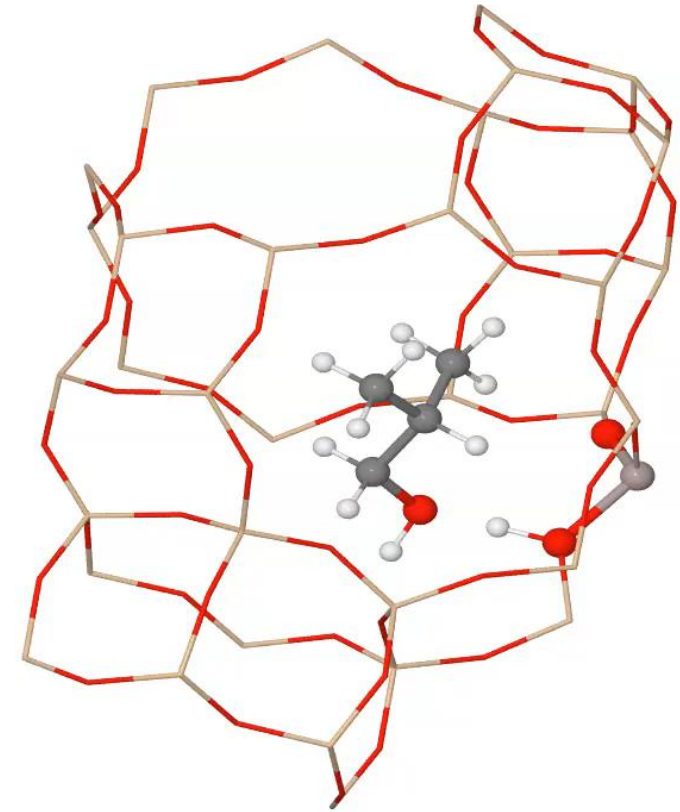
J. Catal. 197 (2001) 68-80

Appl. Catal. B 243 (2019) 594-603

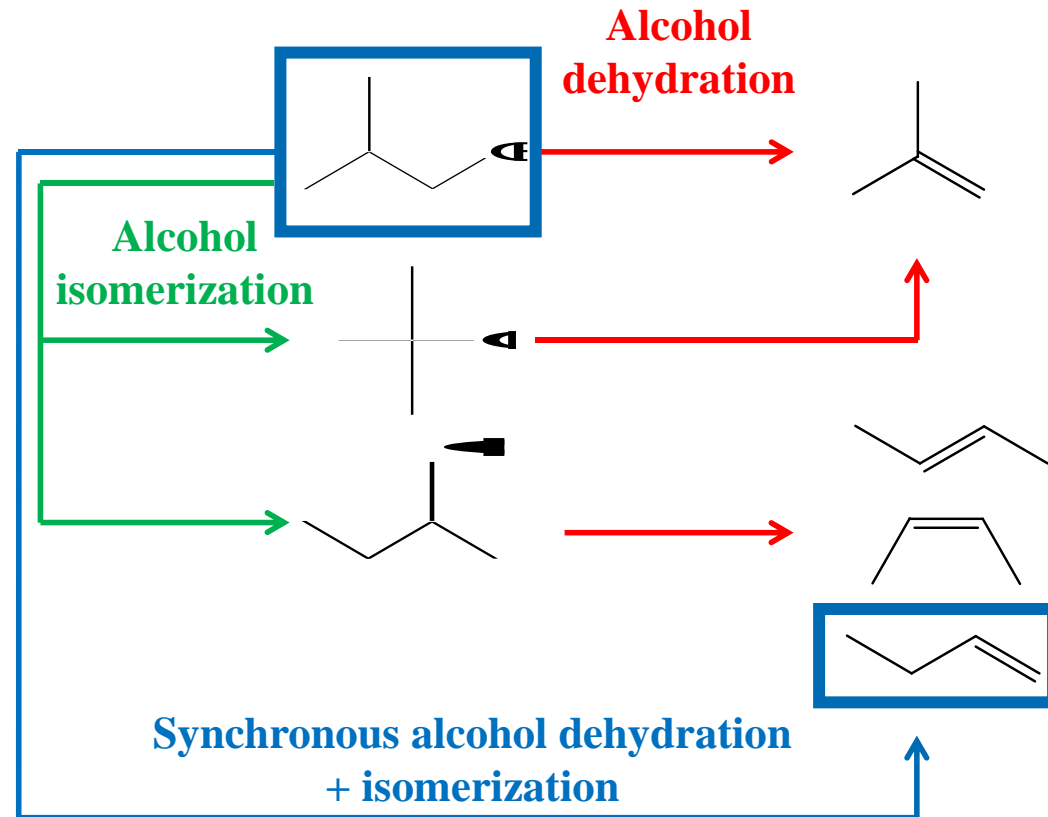
Contradictory results ! How do linear alkenes form ?



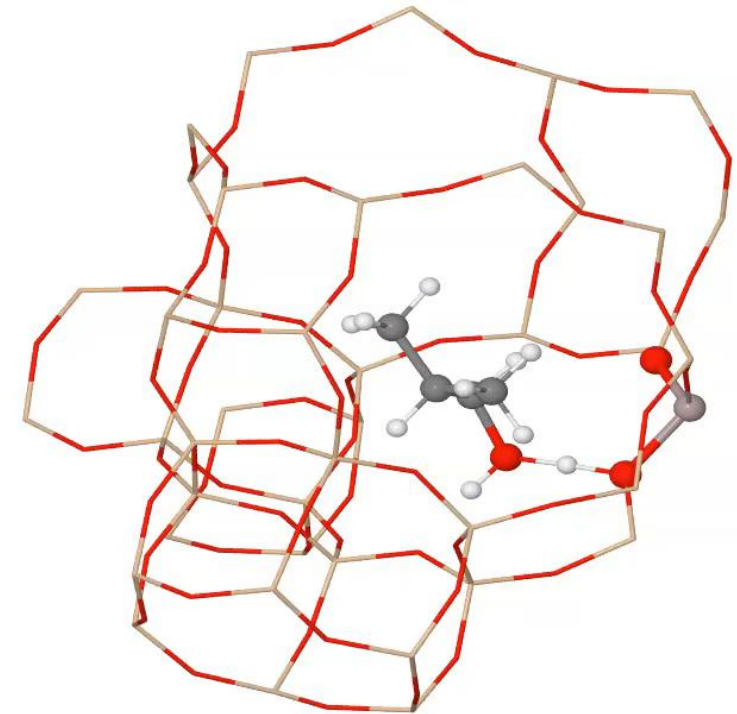
Isomerization of isobutanol into butan-2-ol (CHA):



Intrinsic Reaction Coordinate analysis

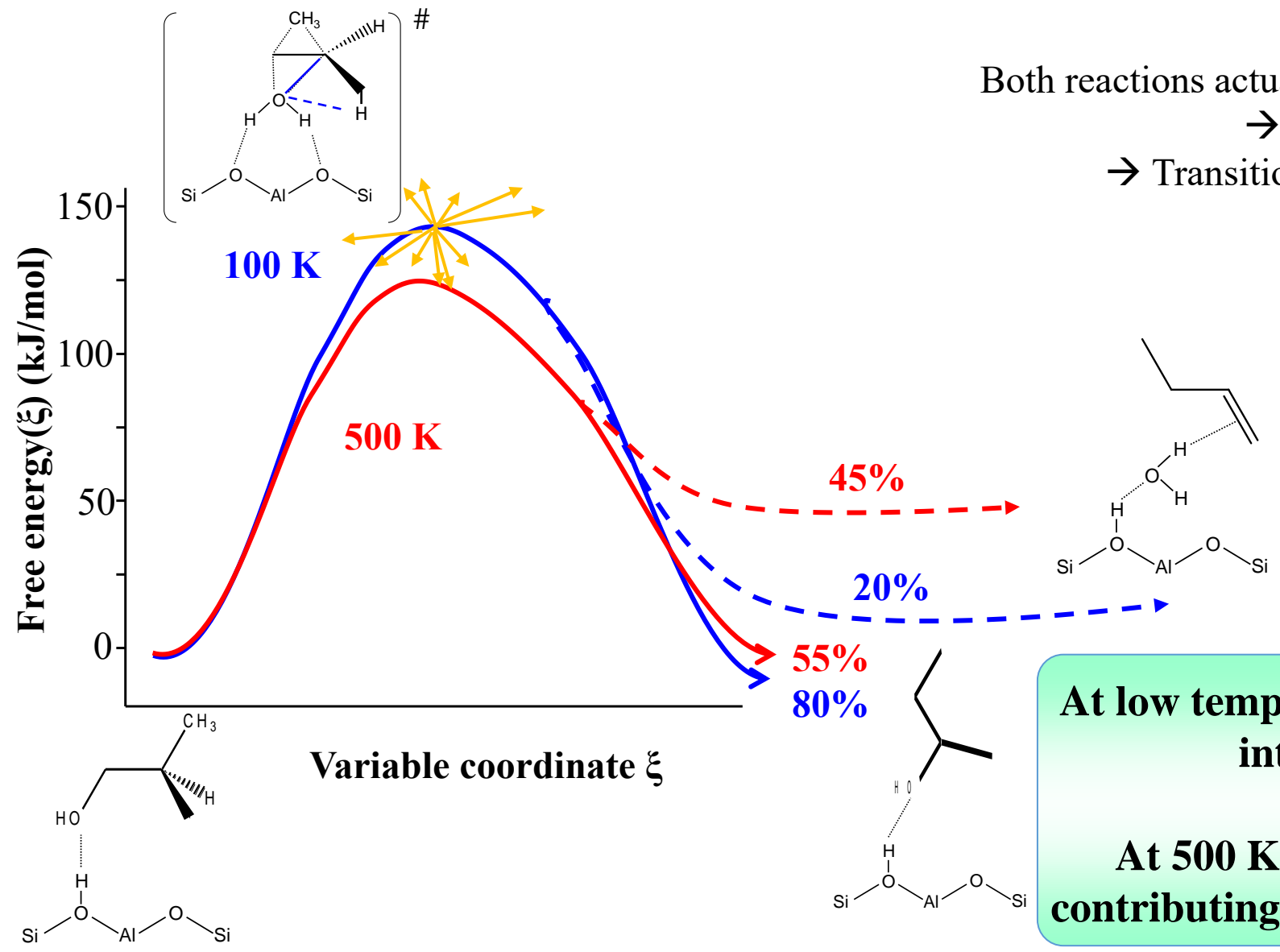


Synchronous isobutanol dehydration and isomerization (CHA):



Intrinsic Reaction Coordinate analysis

COMPETITION BETWEEN ALCOHOL ISOMERIZATION VERSUS SYNCHRONOUS DEHYDRATION/ISOMERIZATION: DYNAMIC EFFECTS



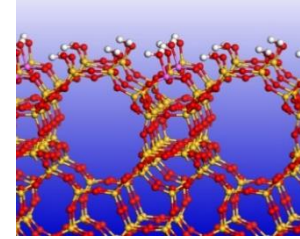
Both reactions actually share a common transition state !
 → Post-TS bifurcation
 → Transition state theory does not apply

At low temperature, isobutanol isomerization into butan-2-ol dominates

At 500 K, both route are nearly equally contributing to the formation of linear alkenes

SIMULATION OF INTRICATE ZEOLITE CATALYSTS

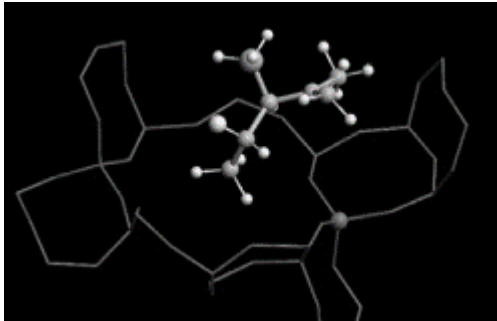
Acid sites at the external surface



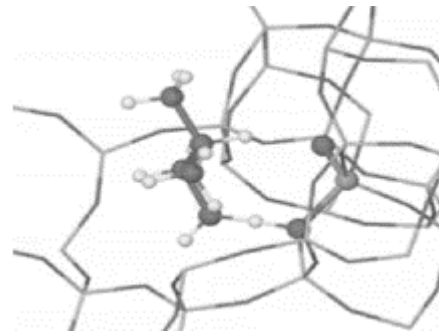
Static investigation of the reactivity of bulk sites

Structural complexity

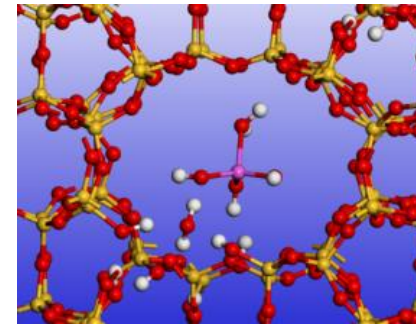
Alkene isomerisation and cracking



Alcohol dehydration



Dealumination mechanisms

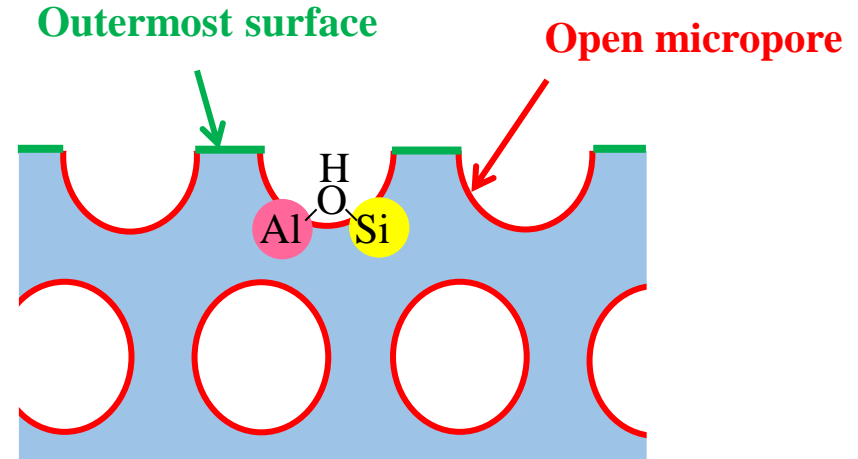
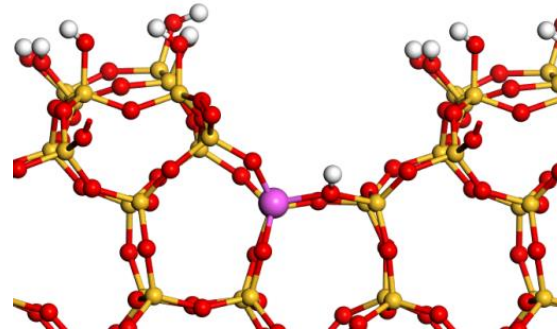


Complexity of chemical reaction investigations

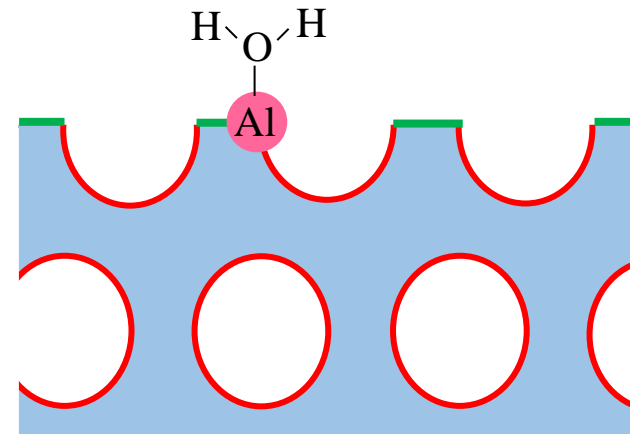
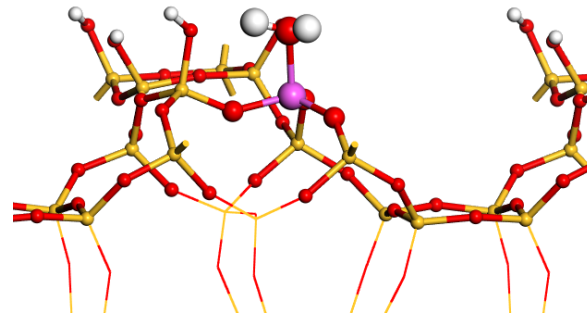
SURFACE MODELS FOR THE EXTERNAL SURFACE OF ZEOLITE BETA AND ZSM-5



Similar stability
as in bulk
micropores:



More stable by
20-60 kJ/mol
than bulk
micropores:



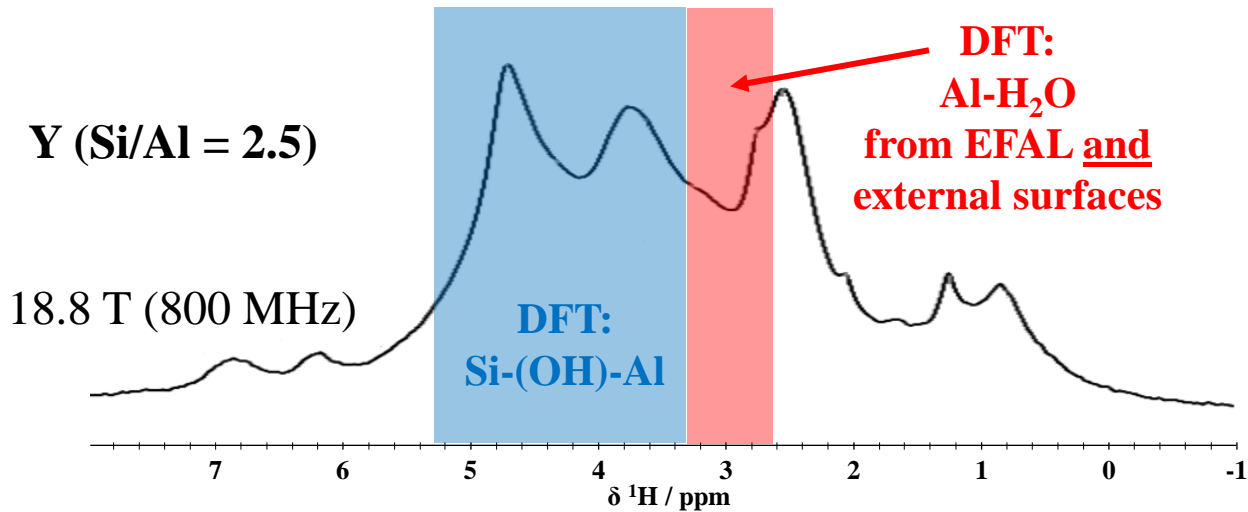
The surface promotes Al-(H₂O) at the outermost surface rather than Si-(OH)-Al

Beta: J. Rey, P. Raybaud, C. Chizallet, *ChemCatChem*, 2017, 9, 2176

ZSM-5: L. Treppe, A. Gomez, T. de Bruin, C. Chizallet, *ACS Catalysis*, 2020, 10, 3297

Faujasite: T. Jarrin, T. de Bruin, C. Chizallet, *ChemCatChem*, 2023, 15, e202201302

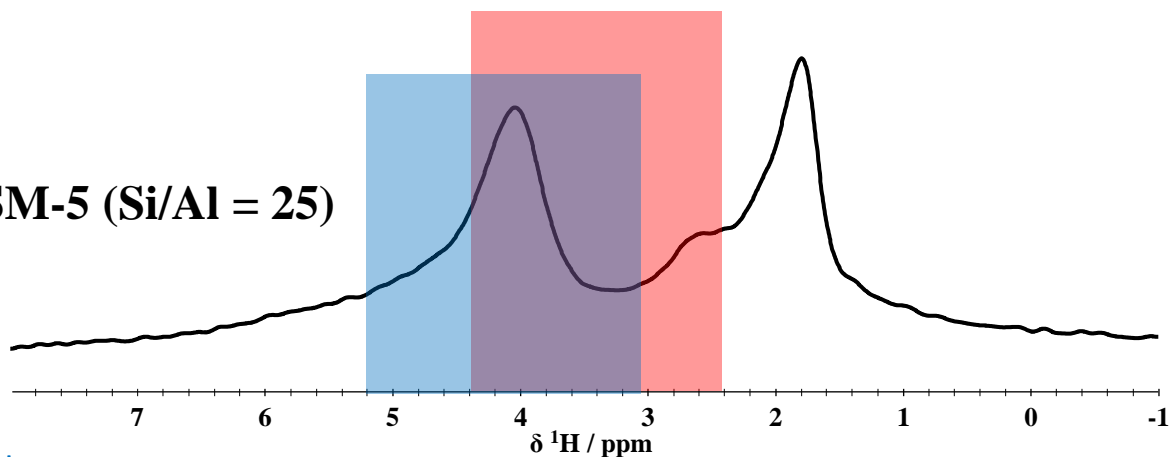
ASSIGNMENT OF ^1H NMR SPECTRA



Usual assignment:

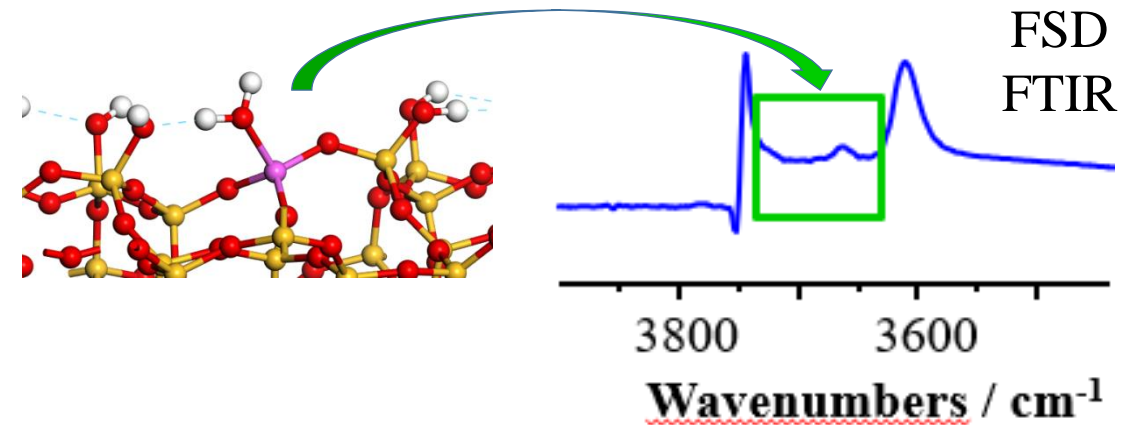


ZSM-5 (Si/Al = 25)



Zones usually assigned to EFALS are not exclusively due to EFALS for both zeolites
Al- H_2O species from external surface also contribute

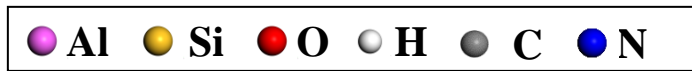
Same observation for FTIR on ZSM-5:



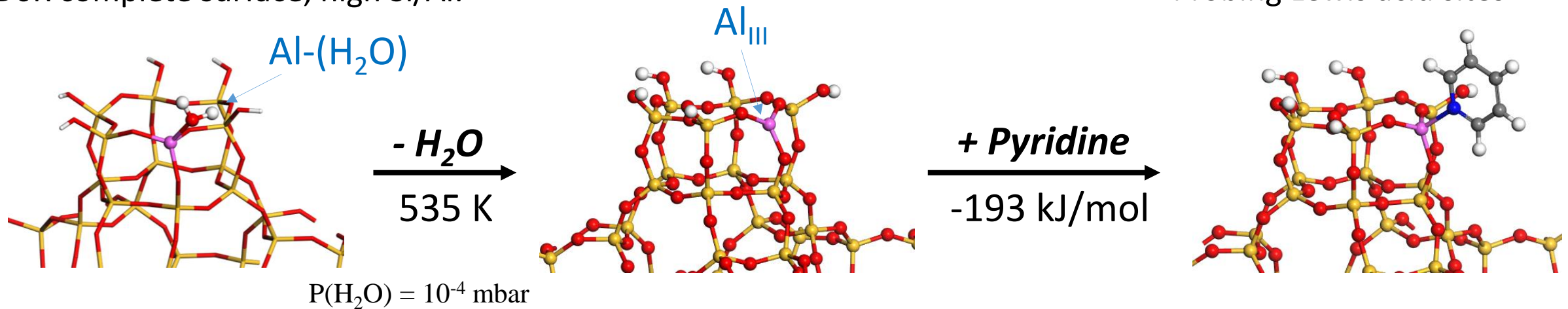
^1H NMR signals usually assigned to Si-(OH)-Al groups are also due to Al- H_2O for ZSM-5

ZSM-5: L. Treps et al. *J. Phys. Chem. C*, **2021**, *125*, 2163
Faujasite: Z. Wang et al., *submitted*

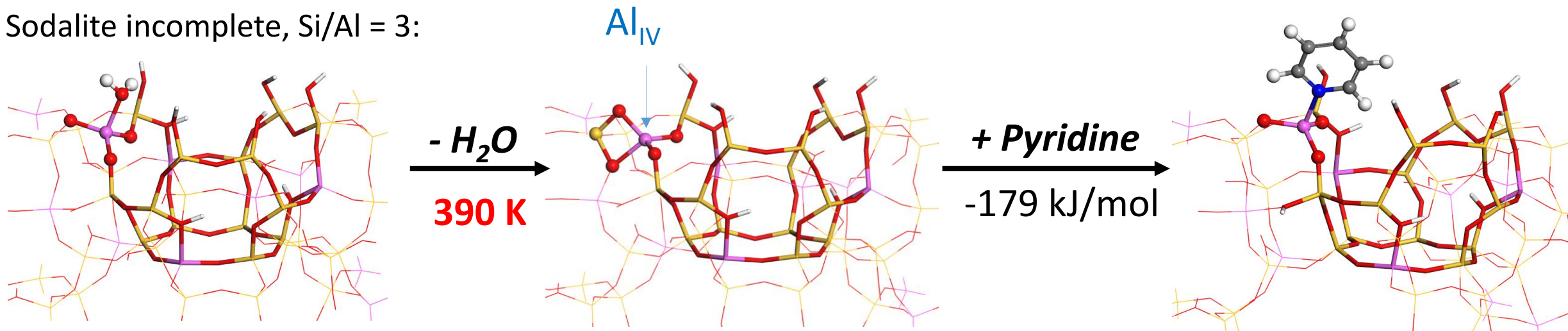
LEWIS ACIDITY OF FAUJASITE



D6R complete surface, high Si/Al:

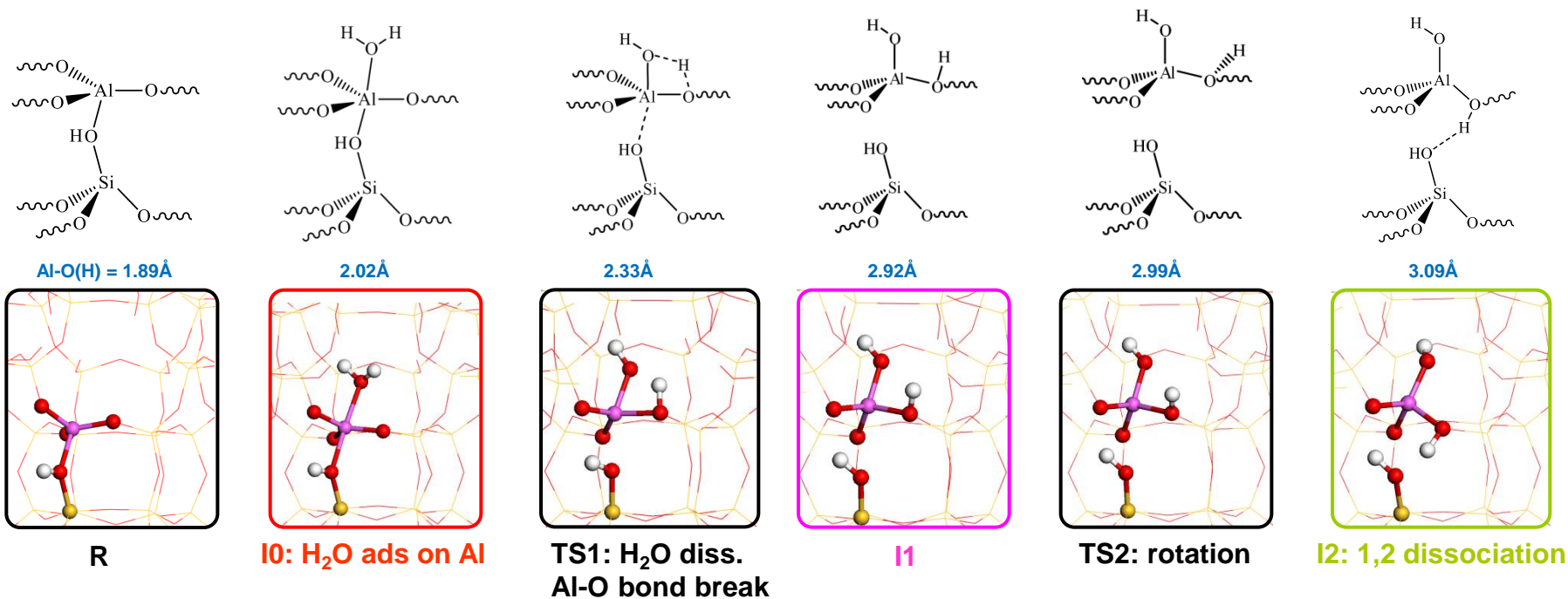


Sodalite incomplete, Si/Al = 3:

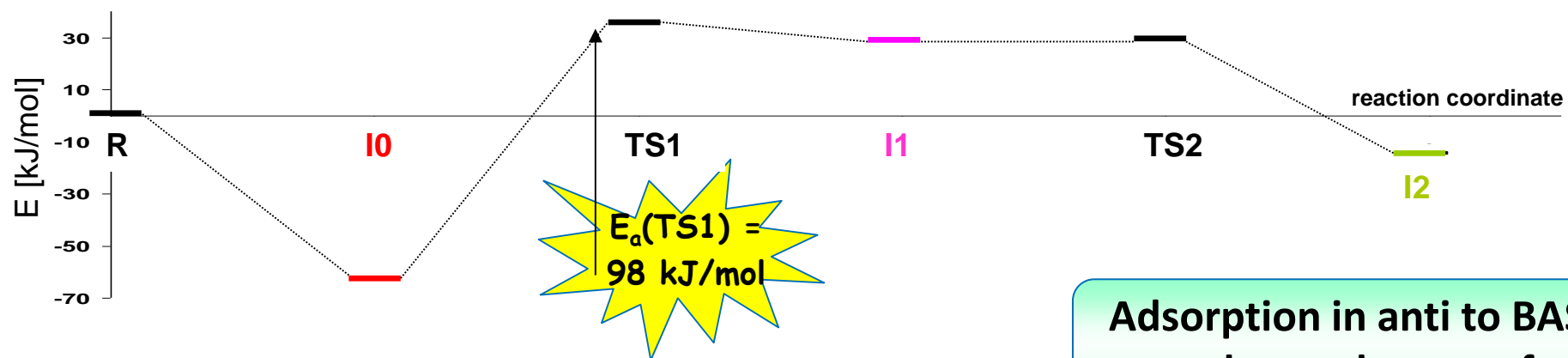


Strong Lewis acid sites are present even in the absence of EFALS on faujasite

DEALUMINATION OF ZEOLITES: FIRST AL-O BOND BREAKING



Ex: TO₁H in FAU

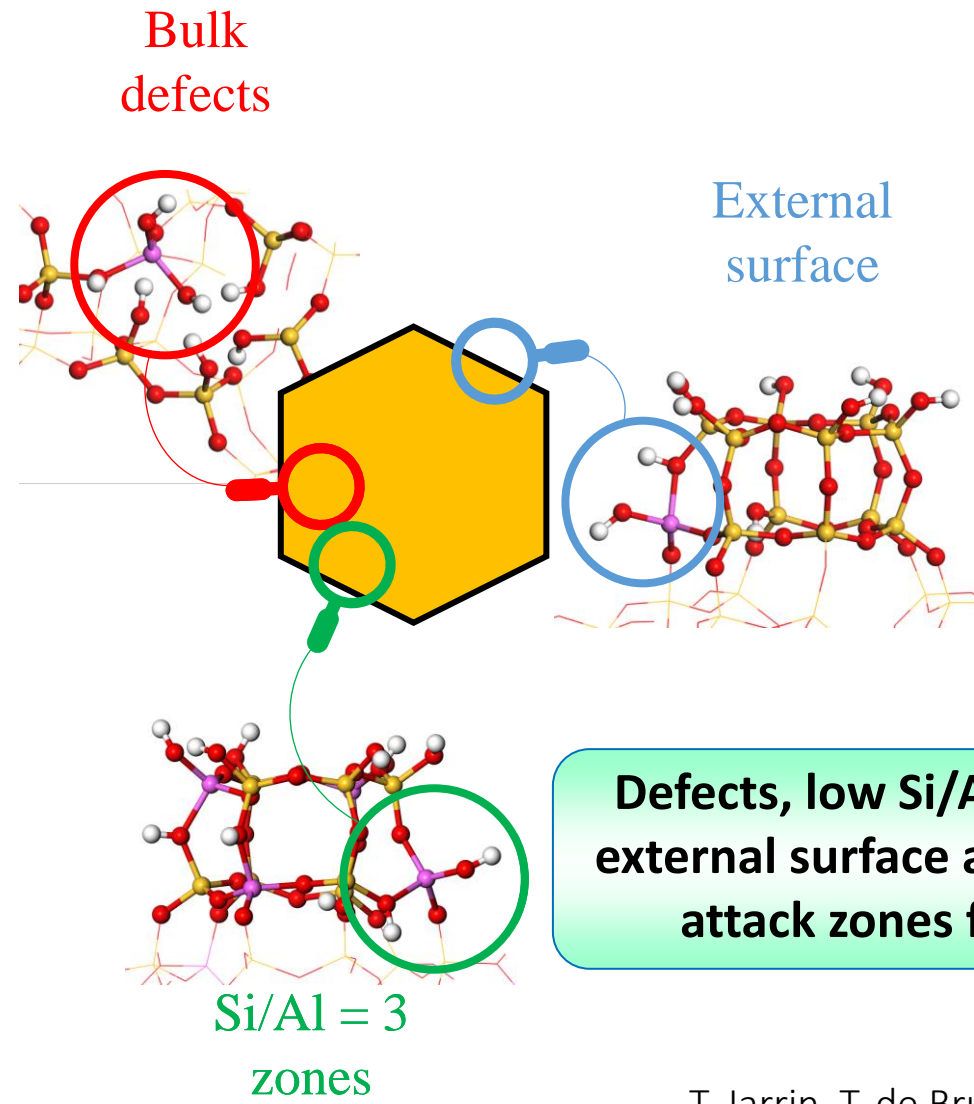
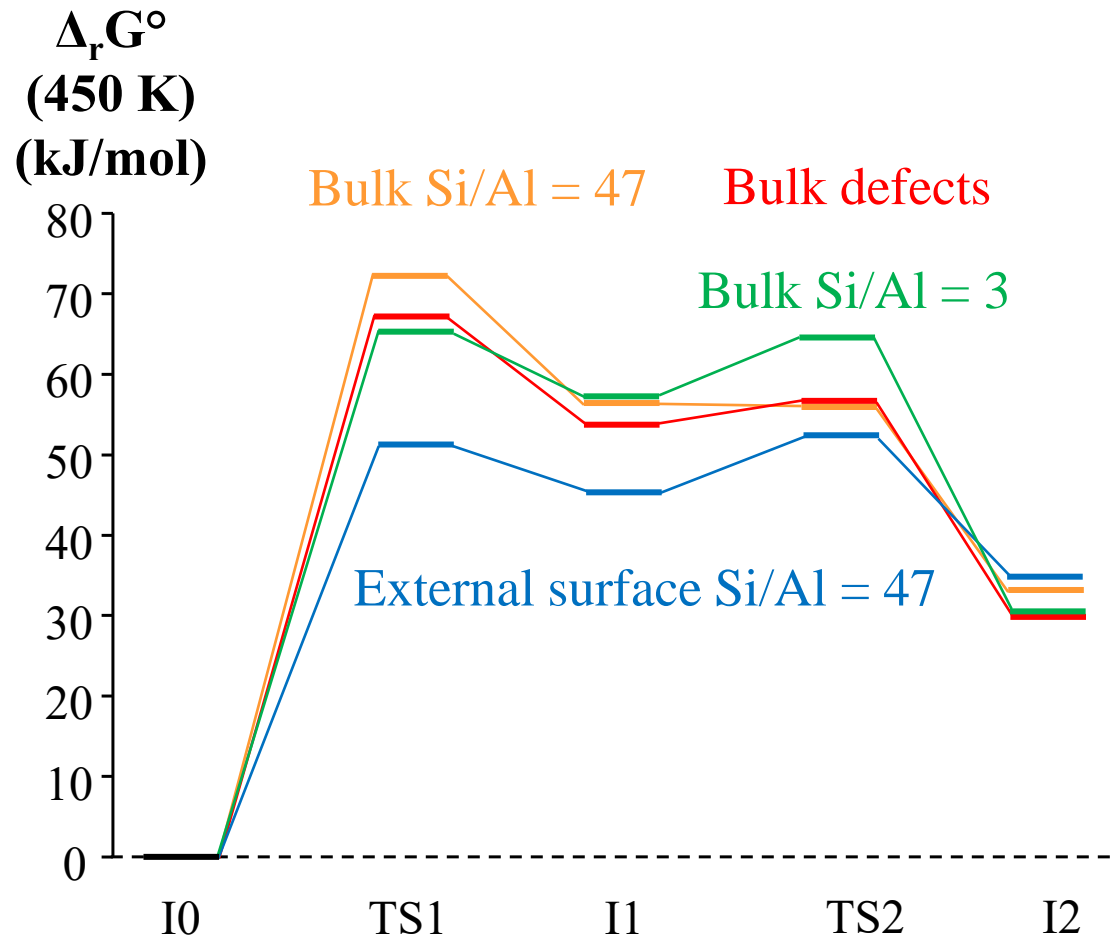


Adsorption in anti to BAS and axial substitution:
always the most favorable mechanism

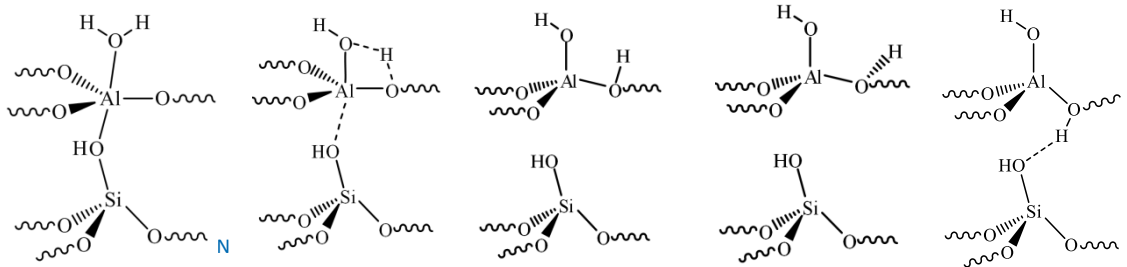


IMPACT OF DEFECTS, SI/AL RATIO AND EXTERNAL SURFACE

TO₃H faujasite



Defects, low Si/Al zones and external surface are preferred attack zones for water



SIMULATION OF INTRICATE ALUMINOSILICATE CATALYSTS: STRUCTURAL AND MECHANISTIC COMPLEXITY

Structural
complexity

Static investigation of the
reactivity of bulk sites

Acid sites at the external surface and
after dealumination are much more
diverse than in the bulk

Ab Initio Molecular Dynamics
and high levels of theory (beyond DFT)
may be necessary to catch the right
mechanisms and rate constants

Next challenges:

- Ever more realistic models for complex catalysts
- Combine structural and mechanistic sources of complexity
- At a higher level of theory to reach chemical accuracy
 - Need of advanced methodologies,
including machine learning

Multi-scale kinetic modeling is feasible in
the field of catalysis by zeolites

Complexity of chemical reaction investigations

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Y. Schuurman



Question and Answer Session



Dr. Alexander Mavromaras

Materials Design



Dr. Céline Chizallet

IFP Energies nouvelles

Questions about Materials Design UGM

Katherine Hollingsworth

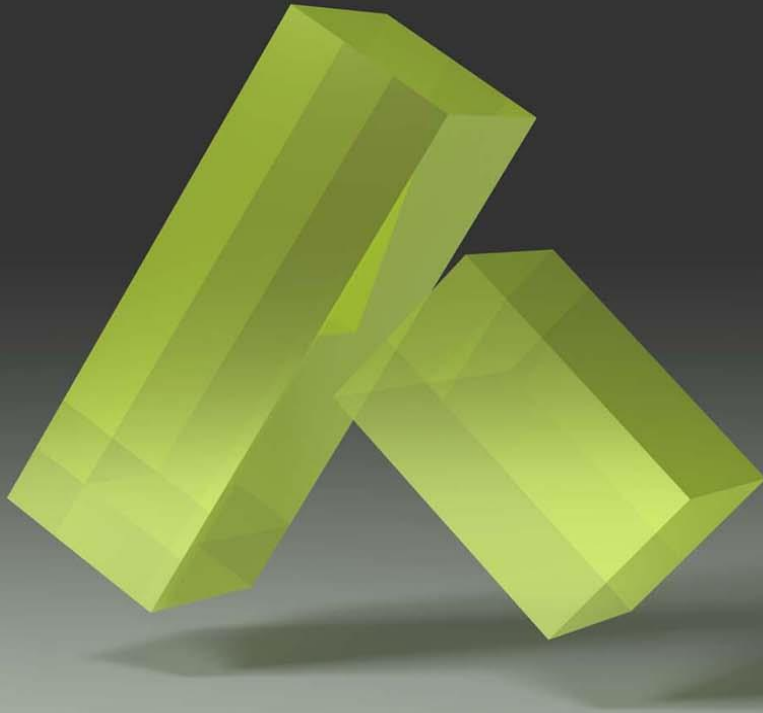
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